

# Resveratrol loaded Pickering emulsions stabilized by OSA modified rice starch granules

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## Abstract

Resveratrol is a photosensitive, bioactive molecule which has received increasing research interest during the past decade for its antioxidant properties. However, it has low solubility in water or common triglyceride oils. Resveratrol solubilization in oil can only be achieved in essential oils, such as flavour oil, but the stability of emulsions produced with this type of oils is low as they are prone to creaming phenomena and Oswald ripening.

In this study, resveratrol was first dissolved in orange oil which was mixed into a medium chain triglyceride (Miglyol) at different ratios and used as the internal phase of oil-in-water emulsions (O/W). The emulsions were stabilized by Octenyl Succinic Anhydride (OSA) modified rice starch granules using two different ratios of starch particle:oil to study the influence of interfacial coverage on final emulsion droplet size and emulsion stability.

The study indicated stable Pickering emulsions could be prepared using OSA-modified rice starch granules even at partial coverage conditions. Emulsions prepared at an oil fraction of 0.5 using 30% v/v mixture of orange oil:Miglyol as the dispersed phase seemed to be an appropriate resveratrol carrier system, obtaining encapsulation efficiency values close to 90% which results in emulsions with a resveratrol concentration of 8.45 mg/L. Hence, the emulsions prepared are suitable for food fortification applications.

**Keywords:** Resveratrol, Pickering emulsions, Rice starch granules, Encapsulation, Orange oil, Emulsion stability

## 1. Introduction

Resveratrol is a natural polyphenol, produced by plants, that is primarily found in the seeds and the skin of grapes and red wine, but it is also present in nuts and berries. Resveratrol shows geometric isomerism, but only trans-resveratrol (trans-3,4,5-trihydroxystilbene), the most abundant form in nature, appears to have biological effects (Hung, et al.,2000, Howitz et al., 2003,Krist, et al., 2009, Machado, et al., 2019). Resveratrol can be considered as a novel nutraceutical which can be used as an ingredient in functional foods to provide consumers with a

34 wide range of benefits such as anti-cancer activity, cardio-protection, antioxidant activity, and  
35 anti-inflammatory activity among others (Machado et al., 2019, Murtaza et al., 2013, Ruivo et al.,  
36 2015, Yang et al., 2014, Saiko et al., 2008). **Although** resveratrol is present in several foods, due  
37 to its low solubility in water and common triglycerides, its absorption is limited (Murtaza et al.,  
38 2013, Novelle et al., 2015). In addition,

39 resveratrol has low chemical stability when exposed to light, high temperature, pH changes, and  
40 some enzymes (Machado et al., 2019, Silva et al, 2013)

41 Microencapsulation is an approach to increase bioavailability and protect unstable bioactive  
42 compounds. Microencapsulation is a process where the bioactive compound is retained within an  
43 encapsulating matrix or membrane. These systems consist of a semipermeable or non-permeable  
44 spherical and strong membrane surrounding a solid or liquid core. **Emulsification** is one of the  
45 common microencapsulation techniques used to encapsulate bioactive compounds (Agustin et al.,  
46 2009).

47 Emulsification involves mixing at least two immiscible phases (usually oil and water), where one  
48 is dispersed in another as droplets. Since this mixture is thermodynamically unstable, the  
49 dispersed droplets tend to merge (coalesce) which in turn will result in destabilization through  
50 phase separation. Therefore, the interface between emulsion droplets needs to be stabilized by  
51 some type of amphiphilic or surface-active compounds, such as surfactants, biopolymers,  
52 and particles. **The emulsion droplets can** be used to encapsulate bioactive compounds for several  
53 industrial applications as cosmetics, food, and pharmaceutical products (Shi et al., 2020; Tang  
54 2020, Matos et al., 2018a).

55 Particle stabilized emulsion, also known as Pickering emulsions, have demonstrated **long-term**  
56 **stability against destabilization** mechanisms such as coalescence and Ostwald ripening. When  
57 particles are at the interface are closely packed, capillary forces are formed between the two  
58 adjacent particles at the same droplet interface what leads to the formation of interfacial pressure  
59 that impedes mass transfer across the interface which in turn, arrest Ostwald ripening (Matos et  
60 al., 2017; Schröder et al., 2017). Moreover, particle-stabilized emulsions have high  
61 biocompatibility compared to emulsions ; stabilized by **surfactants** (Binks, 2001, Matos, et al.,  
62 2016, Marefati., et al., 2017, Marefati, et al. 2018, Albert al., 2019, Tang et al., 2019).

63 Starch particles have been extensively studied for application as Pickering emulsifiers (Timgren,  
64 et al., 2011, Yusoff, & Murray, 2011). Particles should have a partial affinity for both phases (oil  
65 and water) to have efficient stabilizing properties. Since starch particles are naturally hydrophilic,  
66 they need to be modified to optimize their emulsifying efficiency. Starch esterification with  
67 dicarboxylic acids to give Octenyl Succinic Anhydride(OSA) is found to be one of the more

68 effective approaches (Rayner, et al., 2012, Timgren, et al., 2011). A recent study by Marefati and  
69 Rayner (2020) has reported that Pickering emulsions stabilized by OSA modified quinoa starch  
70 granules remained stable for 8 years with no sign of coalescence. However, quinoa starch is not  
71 commercially available which makes other types of starch, such as rice or maize, to have a clear  
72 advantage since they are commercially available. Timgren et al., 2011 and Marefati et al., 2018,  
73 had studied the emulsification properties of several starches and had demonstrated that after  
74 quinoa rice was the type of starch that presented better stabilizing properties.

75 Previously, resveratrol has been encapsulated in nanovesicles (Pando, et al. 2013). Furthermore,  
76 double emulsions have been used for this purpose, in which resveratrol was encapsulated in the  
77 inner aqueous droplets (Matos et al., 2015, Matos et al., 2018b, Gan et al., 2019, Santos, et al.  
78 2019, Shao, et al. 2019). These systems present a clear limitation since the aqueous core can have  
79 the potential affinity to swell and leak into the external aqueous phase (Khadem, et al., 2019).

80 The encapsulation of resveratrol in oil-in-water emulsions has not been largely studied, probably  
81 due to the low oil solubility of the resveratrol. Recent works have been conducted using orange  
82 oil as the oil phase to encapsulate resveratrol obtaining promising results (Davidov-Pardo &  
83 McClements, 2015), with solubilities up to 0.13 mg/g, which is higher than the resveratrol  
84 solubility in pure water (0.03 mg/g).

85 However, emulsion stability was shown to be not very high when orange oil was used as dispersed  
86 phase (Davidov-Pardo & McClements, 2015, Karthik, et al. 2019, Meroni, & Raikos, 2018). The  
87 main reason for this poor emulsion stability is the water solubility of some orange oil components  
88 that favours Oswald ripening phenomena which have found to be decreased by the use of other  
89 hydrophobic compounds in combination with the orange oil (Lim et al. 2011, Meroni & Raikos,  
90 2018, Davidov-Prado & McClements 2015). In all these studies the concentration of orange oil  
91 was found to be very small (5-10% of internal phase), therefore, the knowledge regarding the  
92 effect of higher concentration of orange oil on the emulsion stability is scarce. Moreover, oil-in-  
93 water emulsions used in previous studies as resveratrol carrier presented low oil fraction phase  
94 (10-30% of internal phase), which makes the final resveratrol concentration low despite the high  
95 encapsulation efficiency (Lim et al. 2011, Davidov-Pardo & McClements, 2015, Matos, et al.,  
96 2018a, Matos et al., 2018b).

97 In the present work, the effect of increasing the internal phase concentration of oil-in-water  
98 emulsions formulated using a mixture of orange:Miglyol as oil phase and OSA-rice starch  
99 granules as stabilizer was explored up to their colloidal stability limit using several internal oil  
100 fractions, particles:oil concentration and ratios of orange:Miglyol. Emulsions were characterized  
101 in terms of emulsion droplet size, emulsion stability, and encapsulation efficiency.

## 102 **2. Material and methods**

### 103 **2.1. Materials**

104 Resveratrol (purity is 99%, CAS 501-36-0, MW=228,24 g/mol) was provided by Sigma Aldrich  
105 (USA). The dispersed phase of the emulsions prepared was a mixture of orange oil from Sigma-  
106 Aldrich (USA) and Miglyol 812 from Sasol GmbH (Germany). Native starch granules from rice  
107 grains were supplied by Lyckeby-Culinar AB, Sweden. Starch particles were OSA-modified with  
108 a degree of substitution of 2.7% using the method described by Rayner et al. (Rayner et al., 2012).  
109 As an external continuous phase, for all the emulsions 0.1 M NaCl deionized water solution was  
110 used. The presence of 0.1M NaCl in the aqueous phase was because it has been suggested that  
111 the presence of electrolytes lowers the attractive force between water droplets, decreasing the  
112 dielectric constant of the aqueous phase and therefore reducing collision frequency (Márquez et  
113 al., 2010; Frasc-Melnik et al., 2010; Frasc-Melnik, Spyropoulos et al., 2010; Matos et al., 2018,  
114 Matos et al., 2015). NaCl, methanol of HPLC-grade and absolute ethanol were purchased from  
115 Sigma Aldrich (USA).

### 116 **2.2. Emulsion formulation and preparation**

#### 117 *2.2.1. Formulation with varying concentration of starch*

118 To determine the full coverage conditions, emulsions were prepared at different ratios of  
119 particle:oil varying the OSA-modified rice starch concentrations in the range 100-1000 mg/g (mg  
120 of starch/g oil). The oil volume fractions ( $\phi$ ) selected for these preliminary experiments were 0.1  
121 and 0.3. To eliminate the effect of orange oil on the stability of emulsions, pure Miglyol was used  
122 in this set of experiments. Emulsions were prepared by rotor-stator high shear homogenizer using  
123 a Silent Crusher Mixer (Heildolph, Germany), equipped with 8F type agitator. Firstly, the starch  
124 granules were added to the aqueous solution and mixed by vortex to disperse the starch in the  
125 aqueous phase. Then the oil phase was added. Samples were mixed at 20000 rpm for 1 min, which  
126 was the similar conditions used in previous work when resveratrol loaded quinoa starch Pickering  
127 emulsions were prepared (Matos., 2018b).

#### 128 *2.2.2. Formulations with varying oil volume fractions*

129 To see the effect of different oil fractions on the stability of emulsions, Pickering emulsions with  
130 several dispersed phase volume fractions ( $\phi$ ) (i.e. 0.1, 0.3, 0.4, 0.5 and 0.6) were prepared and  
131 characterized using the emulsification procedure described in section 2.2.1.

#### 132 *2.2.3. Formulations with varying orange oil:Miglyol ratios*

133 To determine the influence of the combination of orange oil with Miglyol as the dispersed phase,  
134 pure Miglyol and mixtures of orange oil:Miglyol in volumetric ratios 1:9 and 3:7 were compared.  
135 Resveratrol was first dissolved in orange oil in a concentration of 0.068 mg/g and mixed for 72

136 h. Davidov-Pardo & McClements 2015, had demonstrated that resveratrol can be dissolved in  
137 orange oil in a concentration of up to 0.13 mg/g. The concentration used in the present work was  
138 close to half of that tested value so their total solubilization could be assumed. The solution  
139 containing resveratrol and orange oil was then mixed with Miglyol as it was reported in previous  
140 work (Matos, 2018b), since Miglyol has been used in formulations of starch stabilized Pickering  
141 emulsions which demonstrated to have high stability (Matos et al, 2016; Timgren et al., 2011).  
142 The final mixture obtained was then used as the dispersed phase using the emulsification  
143 procedure described in section 2.2.1.

### 144 **2.3. Characterization of microstructure of the emulsions**

145 Mastersizer S long bench equipment (Malvern Instruments Ltd., UK) was used to measure the  
146 mean droplet diameter,  $D_{(0,5)}$ , of emulsions prepared and the corresponding droplet size  
147 distributions.

148 Micrographs of the emulsions were also obtained with a light optical microscope (Olympus  
149 BX50, Tokyo, Japan) with 10-40× objective magnifications, with a cover glass on the slide.

### 150 **2.4. Evaluation of emulsion stability**

151 The stability of the emulsions has been measured by Static Multiple Light Scattering (MLS) using  
152 a Turbiscan Lab Expert (Formulation Co. France). The stability of the selected emulsions was  
153 measured at 30° C for 10 days.

154 The Turbiscan Stability Index (TSI) was measured for all samples. TSI is the sum of all the  
155 variations detected in the samples in terms of size and/or concentration, and is defined by equation  
156 1:

$$157 \quad TSI = \sum_i \frac{scan_i - scan_{i-1}}{H} \quad (1)$$

158 where H is the total height of the Turbiscan cell at time intervals i.

### 159 **2.7. Determination encapsulation efficiency (EE)**

160 Resveratrol content in the external aqueous phase was determined by reverse phase high-  
161 performance liquid chromatography (RP-HPLC, HP series 1100 chromatograph, Hewlett  
162 Packard, US). The system was equipped with a UV/VIS absorbance detector HP G1315A and a  
163 fluorescence detector 1260 Infinity A (Agilent Technologies, USA). The column used for the  
164 separation was a reversed-phase column Zorbax Eclipse Plus C<sub>18</sub> of 5 µm particle size, 4.6 mm ×  
165 150 mm (Agilent Technologies, USA). The mobile phase consisted of (A) 100%  
166 MilliQ-water and (B) 100% methanol with gradient elution at a flow rate of 0.8 mL/min. The step

167 gradient started at 80% mobile phase (A) running 100% of the mobile phase (B) in min 5 for 10  
168 min. The mobile phase (B) was running for 2 min after each injection to prepare the column for  
169 the next run. The separation was carried out at room temperature. A wavelength of 305 nm was  
170 used for the UV/VIS detector while the fluorescence detector was used at  $\lambda_{\text{excitation}}/\lambda_{\text{emission}}$  at  
171 310/410 nm. The column was cleaned after each analysis by running the first mobile phase (A)  
172 for 20 min and a mobile phase (C) consisting of 50% acetonitrile, 25% MilliQ-water, 25% 2-  
173 propanol and 0.01% acid acetic for 40 min at a flow rate of 0.25 mL/min. Finally, the column was  
174 rinsed with 50% of the mobile phase (A) and 50% of the mobile phase (B) for another 20 min.

175 The method followed was the one described in precious works (Matos etl al., 2018b) with some  
176 modifications. Emulsions were centrifugated at low speed (1000 rpm for 20 min) in order to  
177 separate the aqueous phase from the oil droplets. The collected aqueous phase was filteredwith a  
178 0.22  $\mu\text{m}$  polyvinylidene difluoride (PVDF) syringe filter, to eliminate all the cream oily phase  
179 residues and any free starch. These filtered samples were then injected into RP-HPLC.

180 As a blank, a sample was prepared for each formulation studied by dissolving the same amount  
181 of resveratrol ina water:methanol solution (volume ratio 1:1) since resveratrol presents poor  
182 solubility in water and the use of methanol will ensure its complete solubilization. Methanol was  
183 not necessary to be added to the aqueous phases recovered from the emulsions since in all cases  
184 the amount of resveratrol collected was lower than the resveratrol solubility in water.

185 The encapsulation efficiency (EE%) was calculated using the following equation:

$$186 \quad \text{EE\%} = \left(1 - \frac{A_s^i}{2 \cdot A_c}\right) \cdot 100 \quad (2)$$

187 where  $A_s^i$  is the area of the peak of the sample detected through RP-HPLC at the day  $i$ , and  $A_c$  is  
188 the area of the blank sample.

## 189 2.8. Statistical analysis

190 Data were expressed as the mean  $\pm$  SD (standard deviation) of three independent experiments,  
191 and statistical analysis of the data was carried out (ANOVA). Fisher's test ( $p < 0.05$ ) was used to  
192 calculate the least significant difference (LSD) using statistical software (Microsoft Excel 2010).

## 193 3. Results

### 194 3.1. Formulations with varying amount of starch

195 In order to determine the full coverage conditions, emulsions were prepared at different ratios of  
196 starch particles:oil. As a general trend, droplet size decreases when the ratio of particle:oil

197 increases until a constant value that indicates that full coverage conditions are achieved  
198 (Tcholakova et al., 2008, Rayner, Timgren et al., 2012). Emulsions with oil fractions of 0.1 and  
199 0.3 were prepared with particle concentrations ranging from 100 to 1000 mg/g (Figures 1A and  
200 1B).

201 Two peaks appeared on all particle size distribution corresponding the smaller one to the presence  
202 of free starch while the larger one to the presence of oil droplets as it was reported in previous  
203 studies (Marefati et al. 2017a and Marefati et al. 2017b, Li et al., 2019). To select the appropriate  
204 starch:oil ratio the mean size of this second peak was studied. A significant droplet size reduction  
205 was observed when a ratio of 400 mg/g was used being the size constant after the addition of 700  
206 mg/g. Similar behavior was observed for an oil fraction of 0.1 and 0.3 when pure Miglyol was  
207 used as the oil phase (Figure 1A, 1B). Previous works, where quinoa starch granules were used  
208 (Matos, et al., 2016) have shown that the minimum ratio of starch particles/oil required necessary  
209 to ensure the stability of the interface oil/water was independent of the oil fraction used.

210 The starch:oil ratio obtained of 700 mg/g was similar to another type of Pickering corn starch  
211 stabilized emulsions (Li et al., 2013) but higher compared to the other types of starch, as is the  
212 case of quinoa starch (Marefati, et al, 2013, Matos, et al., 2018b, Matos, et al., 2016). This is  
213 probably due to the larger size of OSA-rice starch granules which presents a particle size  
214 distribution that varies from 0.5 to 20  $\mu\text{m}$  with a volume weighted mean diameter ( $d_{43}$ ) of 5.2  $\mu\text{m}$   
215 (Li et al. 2013, Sato et al. 2018, Timgren, et al., 2013) compared to OSA-quinoa starch which  
216 presented particle size distributions ranging from 0.5 to 10  $\mu\text{m}$  with a  $d_{43}$  of 2.5  $\mu\text{m}$  (Rayner et al.,  
217 2014), resulting in lower total available area to cover the droplet surfaces at the same mass of  
218 starch compared to quinoa starch granules (Timgren, et al., 2013). So in that sense, two different  
219 starch:oil ratios were selected in order to see the influence of partial and full coverage conditions  
220 (i.e. 400 and 700 mg/g).

221 Figure 1 shows a micrograph of the emulsions prepared with pure Miglyol at 400 (C) and 700 (D)  
222 mg/g. It is possible to see that partially covered emulsion droplets had part of the droplets  
223 uncovered and the initial coalesce can occur while fully covered emulsion droplets present  
224 droplets completely covered by starch particles. Droplet size observed in the micrographs are in  
225 good agreement with the ones obtained by particle size distributions analysis using Mastersizer,  
226 indicating that the larger peak observed was the one responsible of the emulsion droplets.

227 Previous works showed that when orange oil was used as the oil phase a larger amount of starch  
228 is required in order to obtain the oil droplets in full coverage conditions (Matos, et al., 2018b). In  
229 the present work, the ratio of starch:oil was decided to be fixed in the two indicated concentrations  
230 (400 and 700 mg/g) for the three different oil phases studied (pure Miglyol, orange:Miglyol 1:9

231 ratio, orange:Miglyol oil 3:7 ratio). In that sense, the effect of the presence of the orange oil on  
232 emulsions properties could be easily identified.

233 **Figure 1**

234

### 235 ***3.2. Formulations with varying oil volume fractions***

236 Droplet size distribution was measured for emulsions prepared with pure Miglyol as the oil phase.  
237 Figure 2 shows the droplet size distribution of the emulsions using Miglyol as the internal phase  
238 with different internal oil fractions, for the emulsions with partial coverage (400 mg/g) and  
239 complete coverage (700mg/g).

240 **Figure 2**

241 As as aforementioned, for lower  $\phi$  (0.1 and 0.3) the small peak was observed at the lower size,  
242 typically due to the presence of free starch also observed in other works where emulsions were  
243 stabilized by starch particles (Matos et al., 2016, Matos et al., 2018b, Li et al., 2019).

244 At higher  $\phi$  the starch particles probably tended to aggregate producing agglomerates of large  
245 size. This can be the reason why the pick of a few microns was not observed at high  $\phi$  values as  
246 was the case of the work done by other authors (Li et al. 2020) when they study particle size  
247 distributions of starch-stabilized emulsions with  $\phi$  of 0.2-0.6.

248 In both series of samples, it seemed that when  $\phi$  of 0.5 was reached the emulsions started to  
249 change their main droplet size. However, only the emulsions with  $\phi$  of 0.6 seem to had a non-  
250 homogeneous aspect regarding the presence of free oil indicating that the oil was not completely  
251 emulsified. Hence, emulsions reached its colloidal stability limit and the main particle size  
252 distribution started to be divided into two peaks, since coalescence was taking place. Similar  
253 results were obtained by Li et al. (2020) when corn oil was emulsified by quinoa starch, obtaining  
254 satisfactory emulsification up to a  $\phi$  of 0.6. Moreover, Binks et al. (2002) have shown that from  
255  $\phi$  of 0.6-0.7 the emulsion inversion usually takes place when particles are used as stabilizers.

256 It should be pointed out that when  $\phi$  increases the starch particle concentration also increases,  
257 which leads to interparticle interactions and causes the formation of networks of starch and  
258 droplets leading to wider particle size distributions. In addition, the larger oil and starch  
259 concentration of higher  $\phi$  emulsions resulted in a less efficient mixing and hence resulted in wider  
260 particle size distributions merging in a bimodal particle size distribution.



261 Most of the instability phenomena (such as flocculation, creaming, coalescence or Oswald  
 262 ripening) seemed to have their major effect during the first 24 hours (Raikos, 2017, Zhao et al.,  
 263 2014, Meroni & Raikos, 2018)so the stability of emulsions with  $\phi$  of 0.4 and 0.5 was measured  
 264 during 24 hours for emulsions with both starch:oil ratios tested.

265 TSI values were measured being in all cases in the range of 2 to 3.5 units, which indicates high  
 266 stability when compared to other works where this parameter was measured (Raikos, 2017).No  
 267 creaming phenomena wereobserved since the clarification layer was not present. This is probably  
 268 due to the high internal phase concentration that hindrance oil droplets migration to the top of the  
 269 emulsion vessels.Similar behaviour was observed in previous works where high internal phase  
 270 emulsions were prepared with surfactants as the stabilizer (Gutierrez et al., 2014). Droplet  
 271 migration velocity (V) to the surface can be calculated by equation 3 for systems in which the  
 272 internal fraction is medium of high and hence particle movement is affected by the presence of  
 273 their neighboring particles (Snabre & Mills., 1994).

$$274 \quad V = \frac{gd^2(\rho_w - \rho_o)}{18\mu\rho_w} \frac{(1-\phi)}{\left[1 + \frac{4.6\phi}{(1-\phi)^3}\right]} \quad (3)$$

275 where d is the droplet diameter (median size on the volume weighted distribution  $D_{(0.5)}$ ),  $\rho_w$  and  
 276  $\rho_o$ the densities of the continuous phase and dispersed phase respectively,  $\mu$  is the viscosity of the  
 277 continuous phase, g is the gravitational forceand  $\phi$  is the dispersed phase volume fraction.  
 278 However, the use of a large amount of starch as stabilizer increasedthe droplets' densities up to  
 279 values of 1030-1090 kg/m<sup>3</sup> which was similar to continuous phase density, and even larger.  
 280 Hence, not significant migration velocities were expected in the studied systems.

281 For the following experiments, emulsions as dispersed phase mixtures of orange oil and Miglyol  
 282 were used. Emulsions were prepared with  $\phi$  of 0.4 and 0.5.

283 If the internal phase fraction ( $\phi_c$ ) was calculated taking into account, the amount of stabilizer used  
 284 (Equation 4).

$$285 \quad \phi_c = \frac{V_o + V_s}{V_o + V_s + V_w} \quad (4)$$

286 where  $V_o$  is the volume of the oil phase,  $V_s$  is the volume of rice starch and  $V_w$  volume of the  
 287 continuous phase.

288 At 700 mg/g ratio the real internal fraction was larger than at 400mg/g conditions since the amount  
 289 of stabilizer used is higher for the same amount of oil. The real internal phase of emulsions with  
 290  $\phi$  of 0.4 was 0.54 and 0.65 for 400 mg/g and 700 mg/g conditions respectively. While for  
 291 emulsions  $\phi$  of 0.5 the real internal fraction was 0.58 and 0.72 for 400 mg/g and 700 mg/g  
 292 conditions respectively. Hence, an increase of starch concentration in the emulsion could increase

293 oil droplet flocculation within starch networks. Other authors (Li et al, 2019) had studied the  
 294 effect of the degree of substitution of quinoa starch on the emulsification properties observing  
 295 that a low degree substitution showed poor emulsification properties obtaining bimodal  
 296 distributions.

### 297 **3.3. Formulations with different orange oil:Miglyol ratios**

298 Two different orange oil:Miglyol ratios were studied, 1:9 and 3:7 v/v using rice starch as a  
 299 stabilizer for partial and fully covered droplets (400 and 700 mg/g particle:oil ratios). The effect  
 300 of the presence of orange oil mixed in the oil phase on the particle size distribution is presented  
 301 in Figure 3 for emulsions with  $\phi$  of 0.4 and 0.5.

#### 302 **Figure 3**

303 For emulsions with particle:oil ratio of 400 mg/g the addition of orange oil at several  
 304 concentrations seemed to not have an important effect on emulsions size distribution, specially at  
 305  $\phi$  of 0.4. However in the case of  $\phi$  0.5 the presence of orange oil resulted in bimodal size  
 306 distributions.

307 For 700 mg/g formulations, the presence of a high concentration of oil and particles and a low  
 308 amount of water in the formulations resulted in larger sizes at higher oil volume fraction  $\phi$  of  
 309 0.5. On the other hand, the presence of orange oil caused droplet coalescence specially at  $\phi$  of 0.5,  
 310 as it was clearly indicated by the bimodal distribution obtained for emulsions with both orange  
 311 oil concentration tested compared to those with pure Miglyol as the dispersed phase.

312 It seems that the presence of orange oil alters the surface properties of the droplets making the  
 313 particles less efficient for the adsorption at the surface of the droplets. This is in line with the  
 314 previous work (Matos, 2018b), where larger ratio (particles:oil) was required when orange oil  
 315 was present in the oily phase, and hence in the present study coalescence can be taking place due to  
 316 their poor coverage when orange oil was used. The fact that was specially noticeable at a coverage  
 317 ratio of 700 mg/g, since probably at 400 mg/g coalescence was already taking place even when  
 318 no orange oil was used.

319 Theoretical full coverage was also calculated for emulsions, for this purpose. The diameter used  
 320 was the mean value of the peak observed at the particle size distribution that represents the oil  
 321 droplets ( $D_{oil}$ ) since the specific surface area of an emulsion is by definition:

$$322 \quad S = \frac{6\phi}{D_{oil}} \quad (5)$$

323 For full coverage calculations, it was assumed that rice starch particles are spherical and half  
 324 volume of each of them is submerged into the oil phase. The same assumptions were made in  
 325 previous works for theoretical full coverage calculations when starch particles are used (Matos,  
 326 Laca et al., 2018, Timgren, Rayner, Dejmek, Marku, & Sjöö, 2013)

327 Equation 6 was followed to calculate the full coverage of the mass of particles per mass of oil  
 328 ( $\Gamma_{p/o}$ ):

$$329 \quad \Gamma_{p/o} = \frac{N_{p/d} V_p \rho_p}{V_d \rho_{oil}} \quad (6)$$

330 where  $N_{p/d}$  is the number of particles to cover an oil droplet,  $V_p$  and  $V_d$  are the volume of a particle  
 331 and the oil drop respectively and  $\rho_p$  is the density of the starch particles (1.5 kg/L) and  $\rho_{oil}$  is the  
 332 densities of the oils used (0.945 kg/L for pure Miglyol and 0.976 kg/L for a mixture of orange  
 333 oil:Miglyol ratio 1:9 v/v and 0.935 kg/L for a mixture of orange oil:Miglyol ratio 3:7 v/v) and the  
 334  $N_{p/d}$  is calculated by equation 7:

$$335 \quad N_{p/d} = \frac{A_d}{A_{tp}} \quad (7)$$

336 where  $A_d$  and  $A_{tp}$  are the areas of a droplet and the transversal area of a starch particle.

337 Results obtained from theoretical full coverage calculations were shown in Table 1. Theoretical  
 338 full coverage was similar to the ratio of particles:oil used. Only for emulsions prepared with pure  
 339 Miglyol at  $\phi$  of 0.4, theoretical values were much larger than the experimental values used  
 340 indicating that the droplets formed were probably not fully covered by the starch particles.  
 341 However, it is important to point out the wide size distributions obtained, and hence theoretical  
 342 calculations based on mode values can produce some errors on theoretical calculations. Theoretical  
 343 values for emulsions prepared with the ratios of particles:oil of 700 m/g at  $\phi$  of 0.5 were not  
 344 calculated since samples presented extremely wide and bimodal size distributions (Figure 3).

### 345 **Table 1**

346 Figure 4 shows the stability of the formulated emulsions for one week time. All samples presented  
 347 high stability since backscattering profiles remained constant with time. Just a small clarification  
 348 layer was observed at the top part of the cell. Indicating a modest movement of oil droplets to the  
 349 bottom part of the cell. Similar behaviour was observed in previous works (Matos et al., 2016)  
 350 since starch stabilized oil droplets presented higher density than the continuous phase. In the  
 351 mentioned study, the emulsifying ability of starch isolated from quinoa in the granular form, in  
 352 the dissolved state and a combination of both were compared. For this purpose, emulsions  
 353 formulated using Miglyol 812 as oily phase were prepared. When starch granules were used as

354 stabilizer it was observed that at larger ratios of starch particles:oil (200 - 400 mg starch/ml oil)  
355 droplets migrated to the bottom of the cell ,instead of to the upper part, promoted by the  
356 sedimentation of the unadsorbed granules in the continuous phase or small starch granule  
357 stabilized emulsion droplets dense enough to sink due to a large starch to oil ratio, and a density  
358 increase since the relative volume of oil to the starch layer covering it was smaller (Rayner et  
359 al.,2012). Another effect reported caused by the use of high starch concentration was that the  
360 accumulation of starch granules between droplets what also increased their total effective density  
361 (Timgren et al., 2013).

362 Previous works verified the Oswald ripening behaviour observed when orange oil was used due  
363 to their partial water solubility (Zhang et al, 2015, Raikos 2017, Meroni & Raikos, 2018). On the  
364 otherhand, some authors have observed that Oswald ripening was hindered when orange oil was  
365 encapsulated in other more lipophilic carrier oils. Carrier oils demonstrated an Oswald ripening  
366 inhibition effect by the generation of entropy mixing which was found more thermodynamically  
367 stable (Meroni & Raikos, 2018, Zhang, 2015). The favourable effect of entropy mixing seemsto  
368 be present in this study since all emulsions formulated demonstrated to have high stability which  
369 could be the explanation of their high stability. Any significant increase on droplet size was  
370 observed over time (Lemarchand et al., 2003).

371 It is important to point out that the mean oil droplet sizes of the emulsions in the present study  
372 were considerably larger than the one measured in previous works, in which surfactant or proteins  
373 were used to stabilize orange oil-in-water emulsions (Meroni & Raikos, 2018, Zhang, 2015, Zaho  
374 et al. 2014, Davidov-Pardo & Mc Clements 2015),being even larger than other works were other  
375 types of starch were used as a stabilizer (Li et al., 2013). This is due to the larger particle sizes of  
376 rice starch granules, as explained earlier, and the high particle concentration which could result  
377 in the formation of aggregated network of droplets due to interparticle interactions.

378 In that sense, the oil migration due to the density difference between the oil and the aqueous  
379 phases could be more favourable in this study. However, the larger internal phase concentration  
380 raised in this work, compared to previous works (Meroni & Raikos, 2018, Zhang, 2015, Zaho et  
381 al. 2014, Davidov-Pardo & Mc Clements 2015, Li et al., 2013), could limit droplet movement due  
382 to their higher viscosity.

383 **Figure 4**

### 384 *3.4 Encapsulation of resveratrol*

385 Emulsions with  $\phi$  of 0.5 were selected for this resveratrol encapsulation since even the wider  
386 droplet size distribution achieved for this formulation was not exceeding the 200  $\mu\text{m}$  and had  
387 shown high stability. Taking into account that the concentration of resveratrol on orange oil was

388 kept constant (0.068 mg/g). The use of  $\phi$  of 0.5 could produce final emulsions with a resveratrol  
389 concentration of 0.0034 and 0.0102 mg/g for orange:Miglyol ratio 1:9 and 3:7, respectively. On  
390 the contrary, the use of  $\phi$  of 0.4 could produced final emulsions with a resveratrol concentration  
391 of 0.00272 and 0.00816 mg/g for orange:Miglyol ratio 1:9 and 3:7, respectively. Hence the  
392 selection of a  $\phi$  of 0.5 offers a potential clear advantage for further emulsion applications.

393 The results of the effect of the two different internal phase ratios of orange:Miglyol oil phase(1:9  
394 and 3:7) and two different ratios of starch:oil, 400 and 700 mg/g are presented in Figure 5.

395 As a general trend it can seen that the increase of orange oil concentration and the increase of  
396 starch/oil ratio increased encapsulation efficiency. However, significant differences encapsulation  
397 efficiency were observed for emulsions with orange:Miglyol ratio of 3:7 and a ratio of starch:oil  
398 of 700 mg/g respect and emulsion with orange:Miglyol ratio of 1:9 and a ratio of starch:oil of 400  
399 mg/g, with values of 89% and 81 % respectively. The fact that emulsion with orange:Miglyol  
400 ratio of 3:7 and a ratio of starch:oil of 700 mg/g had bimodal and wider size distribution did not  
401 negatively affect the encapsulation capacity of the emulsions. Not significant differences were  
402 observed when the orange oil ratio was increased at a constant starch/oil ratio and for and increase  
403 of the starch/oil ratio at a constant orange oil concentration, indicating a synergic effect between  
404 both variables.

405 All emulsions showed high encapsulation efficiencies (larger than 80%), being the encapsulation  
406 efficiency values higher than those previously obtained for the similar formulation when  
407 surfactant Tween 20 or whey isolated proteins were used as the stabilizer (values around 60%  
408 were registered) (Sha et al., 2019; Bao et al., 2020; Chen et al., 2020). However, similar values  
409 obtained when quinoa starch particles were used (values around 80-95% were registered) (Matos  
410 et al., 2018). However, even the EE values are quite similar to the ones obtained with quinoa starch  
411 , the high content of internal oil fraction and orange oil in the oil phase increase resveratrol  
412 concentration from 1.72 to 8.45 mg/L.

413 A recent study reported encapsulation efficiencies up to 97% for systems prepared by membrane  
414 emulsification and further spray drying using palm oil as oil phase, the final resveratrol  
415 concentration on the obtained powder was 0.8 mg/g (Consolo et al., 2020). Other type of  
416 emulsions such as gel filled emulsions reported maximum resveratrol encapsulation efficiencies  
417 up to 60%. Encapsulation efficiencies close to 90% were also reported when resveratrol was  
418 encapsulated in double emulsions, being resveratrol entrapped in that case in an ethanolic internal  
419 aqueous phase (Diaz-Ruiz et al., 2020)

420

421

**Figure 5**

422 Stability of all emulsions were recorded for ten days to study the effect of different concentration  
423 orange oil in the dispersed phase mixture used on the emulsion stability for partial and full  
424 coverage formulations with and without encapsulated resveratrol. Backscattering profiles are  
425 presented in Figure 6.

426 **Figure 6**

427 In general terms, from the stability backscattering profiles a clarification layer at the top part,  
428 higher than the registered in samples without resveratrol could be observed (figure 4). The results  
429 obtained, indicated that the presence of resveratrol slightly negatively affected the stability of the  
430 emulsion. Clarification at the top part of the cell occurred in all samples and differences on the  
431 backscattered light in the middle part of the cell indicated growth of the droplet size.

432 The negative effect of the presence of resveratrol on the stability could be due to the migration of  
433 resveratrol to the surface of the droplets as was observed by other authors (Davidov-Pardo &  
434 McClements, 2015) that may alter the interfacial activity of the droplets.

435 In the present study, the backscattering variations observed were not high and TSI values lower  
436 than 15 were recorded in all cases, indicating high stability.

#### 437 **4. Conclusions**

438 Pickering emulsions with an oil fraction of maximum 0.5 stabilized by OSA- modified rice starch  
439 granules showed high stability against creaming phenomena. Homogenous and stable emulsions  
440 with higher internal phase were not possible to be obtained with the equipment and operating  
441 conditions used in the present study.

442 Oil droplets with partial coverage of OSA- modified rice starch granules showed high stability  
443 indicating that it is not necessary to have full coverage conditions. However, larger mean droplet  
444 size was observed for these formulations.

445 Orange oil can be used up to a 30% v/v in combination with Miglyol as the oil phase to obtain  
446 emulsions with high stability. However, the use of orange oil as a portion of the oily phase  
447 increased the mean droplet sizes of the resulting emulsions.

448 Pickering emulsions stabilized by OSA- modified rice starch granules using a mixture of orange  
449 oil in combination with Miglyol as the dispersed phase seemed to be an appropriate resveratrol  
450 carrier system, obtaining resveratrol encapsulation efficiency values up to  $89 \pm 2.3\%$  which  
451 corresponds to a concentration of 8.45 mg/L on the final emulsions. The system formulated could  
452 be considered suitable for further use in functional food formulations.

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- 630
- 631
- 632

## Highlights

- OSA-rice starch Pickering emulsions containing Resveratrol were prepared
- Stable Pickering emulsions with internal volumetric fraction up to 50% were prepared
- Orange oil was used as Resveratrol carrier in the oily phase
- Stable emulsions with 30% of orange oil on the oily phase were prepared
- OSA-rice starch Pickering emulsions contained 8.45 mg/L of Resveratrol (90% EE)

## Figure Captions

Figure 1. Particle size distribution of emulsions prepared at several starch/Miglyol ratio,  $\phi$  of 0.1 (A) and  $\phi$  of 0.3 (B). Microscope images of emulsions formulated with pure Miglyol 812 as dispersed phase stabilized with OSA-modified rice starch granules at 400 mg/g (C) and 700 mg/g (D) conditions with  $\phi$  of 0.3.

Figure 2. Emulsion particle size distributions with different oil fractions (0.1 to 0.6) at partial (400 mg/g) and full coverage (700 mg/g).

Figure 3. Effect of the presence of orange oil on the droplet size distribution of the emulsions. M: Pure Miglyol, O+M (1:9): orange oil:Miglyol ratio (1:9 v/v) and O+M (3:7): orange oil:Miglyol ratio (3:7 v/v)

Figure 4. Backscattering profiles of emulsions with 400 and 700 mg/g of starch:oil and ratios 1:9 and 3:7 or orange oil:Miglyol during 10 days. All samples contain internal oil fraction of 0.5

Figure 5. Encapsulation efficiency of resveratrol in emulsions with different oil ratios and partial and full coverage conditions

Figure 6. Backscattering profiles of resveratrol loaded emulsions with 400 and 700 mg/g of starch:oil and orange oil:Miglyol ratios of 1:9 and 3:7 or during 10 days. All samples contain internal oil fraction of 0.5.

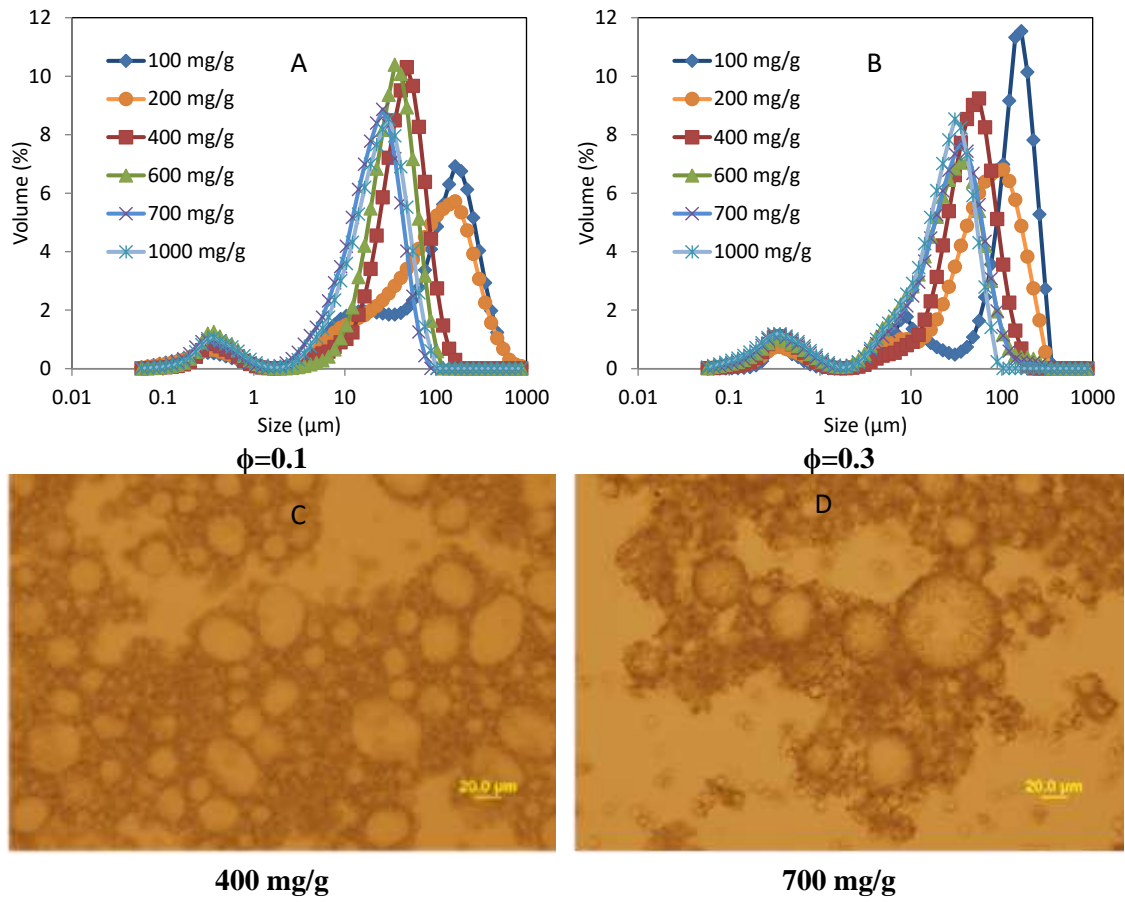


Figure 1

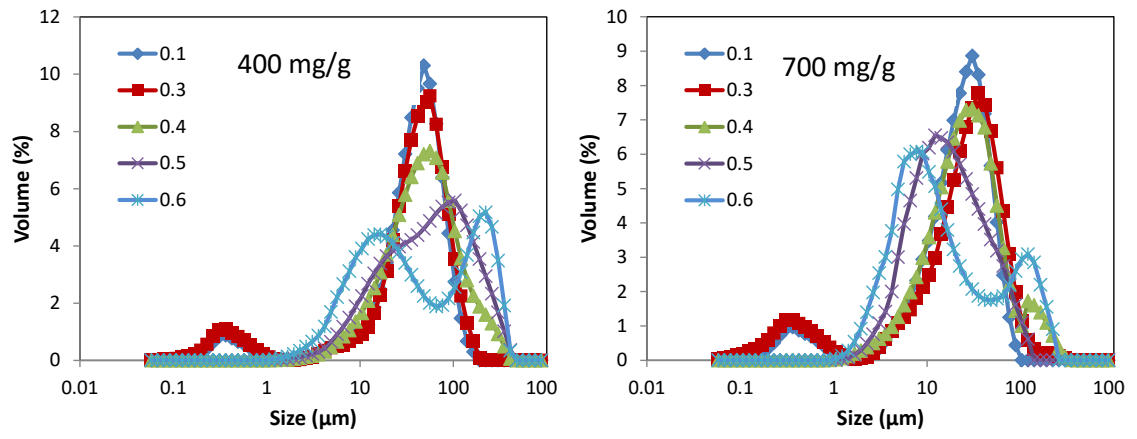
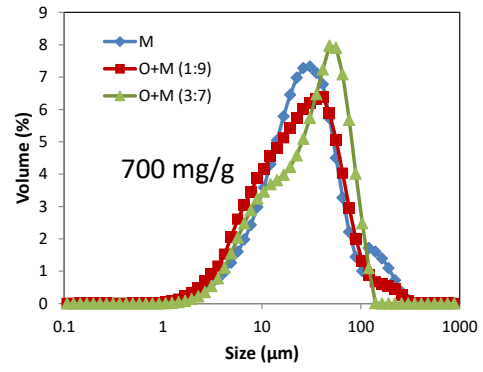
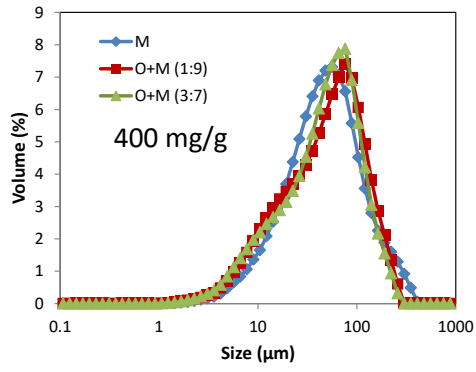
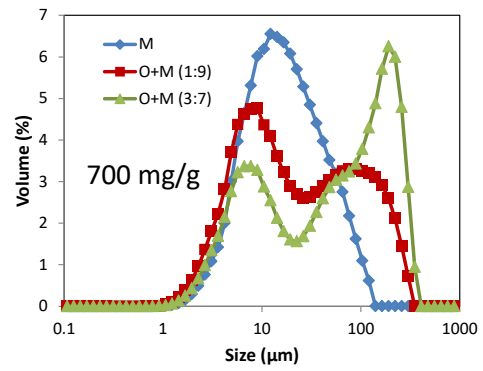
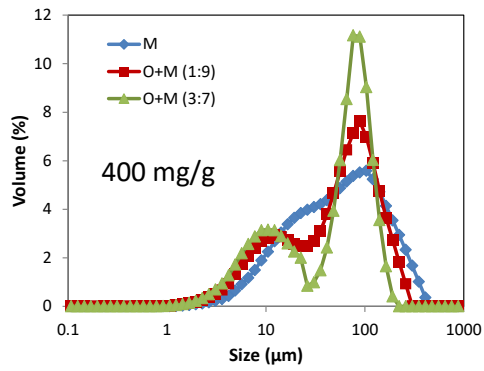


Figure 2



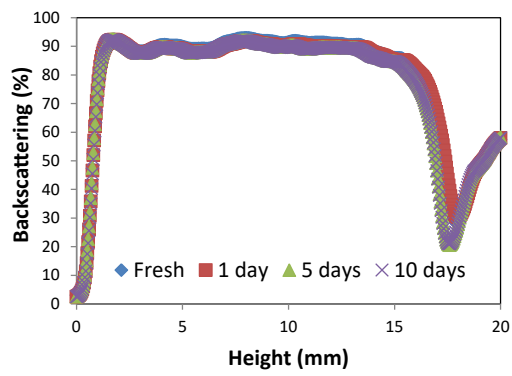


$\phi=0.4$

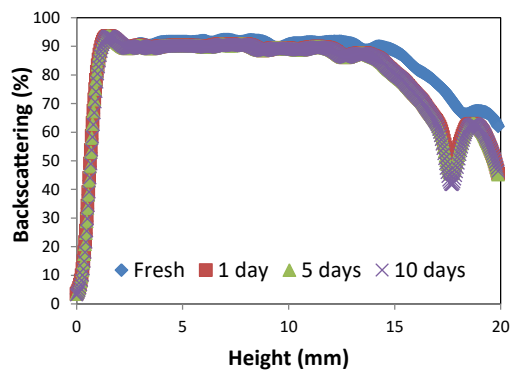


$\phi=0.5$

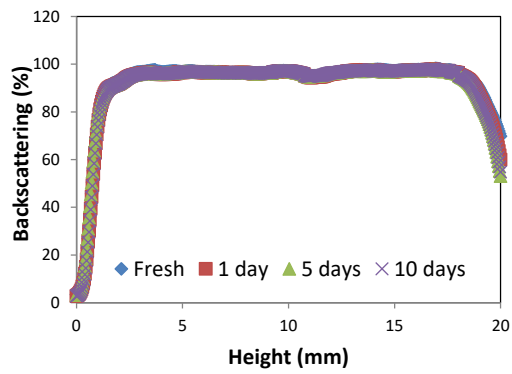
Figure 3



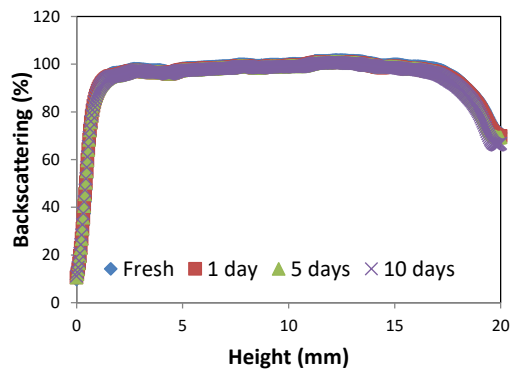
400 mg/g, orange:Miglyol, 1:9



700 mg/g, orange:Miglyol, 1:9



400 mg/g, orange:Miglyol, 3:7



700 mg/g, orange:Miglyol, 3:7

Figure 4

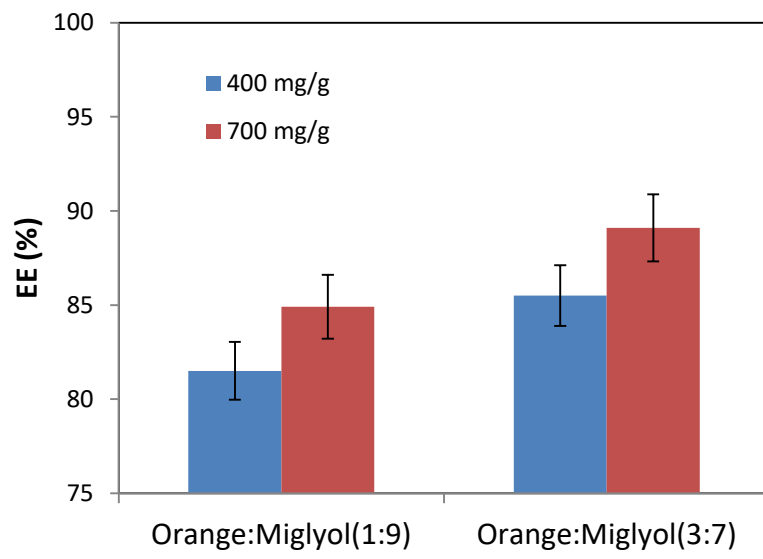
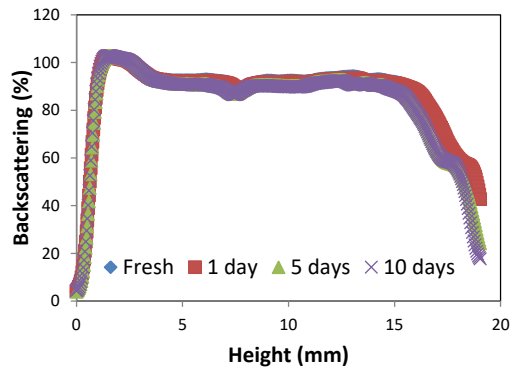
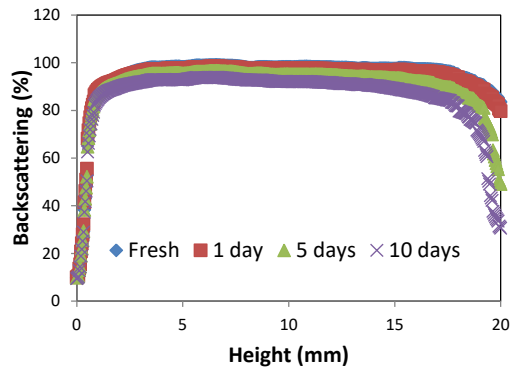


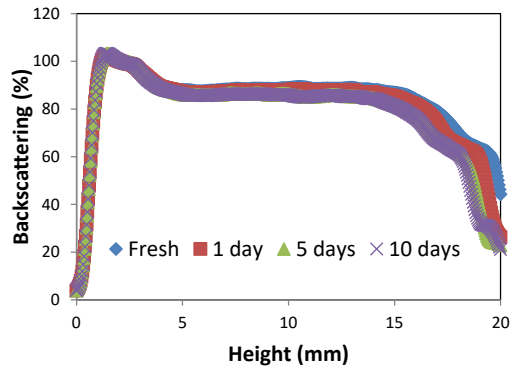
Figure 5



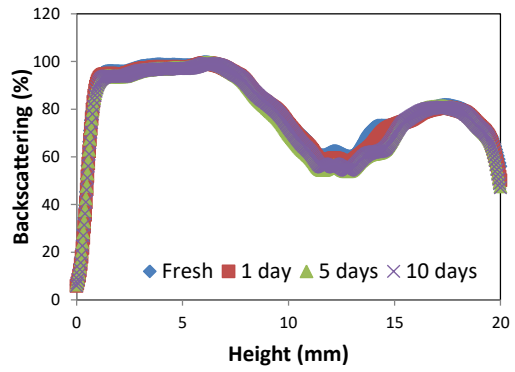
400 mg/g, orange:Miglyol, 1:9



700 mg/g, orange:Miglyol, 1:9



400 mg/g, orange:Miglyol, 3:7



700 mg/g, orange:Miglyol, 3:7

Figure 6

Table 1. Theoretical full coverage and surface particle size for emulsions prepared at internal oil phase fraction of 0.4 and 0.5

<b>Coverage used 400 mg/g</b>						
<b>Miglyol</b>		<b>Orange:Miglyol (1:9)</b>		<b>Orange:Miglyol (3:7)</b>		
<i>mode</i>	$\Gamma_{p/d}$	<i>mode</i>	$\Gamma_{p/d}$	<i>mode</i>	$\Gamma_{p/d}$	
( $\mu\text{m}$ )	(mg/g)	( $\mu\text{m}$ )	(mg/g)	( $\mu\text{m}$ )	(mg/g)	
$\phi=0.4$	48.3	717	76.3	454	76.3	454
$\phi=0.5$	76.3	454	75.8	457	76.7	452
<b>Coverage used 700 mg/g</b>						
<b>Miglyol</b>		<b>Orange:Miglyol (1:9)</b>		<b>Orange:Miglyol (3:7)</b>		
<i>mode</i>	$\Gamma_{p/d}$	<i>mode</i>	$\Gamma_{p/d}$	<i>mode</i>	$\Gamma_{p/d}$	
( $\mu\text{m}$ )	(mg/g)	( $\mu\text{m}$ )	(mg/g)	( $\mu\text{m}$ )	(mg/g)	
$\phi=0.4$	26.2	1322	35.6	976	48.27	718