Long-term thermal stability of fatty acid anion-based ionic liquids

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Abstract

Isothermal and dynamic methodologies were used to study the thermal degradation of 8 novel fatty acid anion-based ionic liquids (FAILs): methyltrioctylammonium hexanoate $[N_{8,8,8,1}][C_{6:0}]$, methyltrioctylammonium octanoate $[N_{8,8,8,1}][C_{12:0}]$, tetrahexylammonium octanoate $[N_{8,8,8,1}][C_{12:0}]$, methyltrioctylammonium palmitate $[N_{8,8,8,1}][C_{12:0}]$, methyltrioctylammonium palmitate $[N_{8,8,8,1}][C_{12:0}]$, methyltrioctylammonium stearate $[N_{8,8,8,1}][C_{16:0}]$, tetrahexylammonium stearate $[N_{8,8,8,1}][C_{16:0}]$, and methyltrioctylammonium oleate $[N_{8,8,8,1}][C_{18:1}]$.

The thermal stability of these FAILs is controlled by both the cation and anion and most samples have an onset decomposition temperature (T_{onset}) below 200 °C. All the FAILs exhibited lower thermal stability under a nitrogen atmosphere than commercially available ILs tested previously in lubrication studies, particularly when compared to those containing the $[NTf_2]^-$ anion. The $[N_{8,8,8,1}][C_{6:0}]$ and $[N_{8,8,8,1}][C_{8:0}]$ showed the highest long-term thermal stability, probably related to their stronger anion-cation electrostatic interaction. This led to a multi-step thermal decomposition mechanism observed in the DTG results. Finally, isoconversional modelling for the $[N_{8,8,8,1}][C_{12:0}]$ agrees with isothermal results.

Keywords: fatty acid ionic liquids; thermogravimetric analysis; isothermal thermogravimetry; isoconversional method; model-free kinetics.

1. Introduction

A salt in the liquid state is usually called an ionic liquid (IL), ethylammonium nitrate [(C₂H₅)NH₃][NO₃] being the first IL reported at the beginning of the last century [1]. More specifically, the term IL used to be restricted to salts whose melting point is below 100 °C. While ordinary liquids are predominantly composed of electrically neutral molecules, ILs are compounds largely made up of ion pairs: bulky organic and asymmetric cations combined with a variety of small inorganic or organic anions [2, 3] and this characteristic grants them very interesting properties, such as: extremely low volatility, large liquid ranges and low melting temperature, among others. Furthermore, this variety of physicochemical and thermodynamic properties depends on their cation-anion combinations, which means that they are appropriate for a wide range of applications, due to the large number of cation-anion combinations that are available [4-15].

The idea of employing ILs in lubrication was studied for the first time in 2001 [16] and subsequent research has continued to show promising results [5, 17-20]. The most common ILs used in the early research were based on the $[PF_6]^-$ and $[BF_4]^-$ anions [21-23]; but corrosion issues were detected [24-28] and more stable

fluorine-based ILs containing [FAP]⁻ and [NTf₂]⁻ anions with excellent tribological properties started to be studied in order to avoid the mentioned corrosion problems [28-45]. On the other hand, new families of ILs have been synthesized recently, with the objective of simultaneously achieving low toxicity and high biodegradability [46-52]. A metathesis reaction for the obtention of ionic liquids from fatty acids (fatty acid ionic liquids or FAILs) was firstly reported in 2013 [53]. Then, these FAILs began to be used increasingly in lubrication studies [54-70], which reported that their thermal behaviour was poorer than that of the "conventional" (or commercially available) ionic liquids.

Thermal stability is an important property when considering the application of ILs in lubrication. Although a lot of research into the thermal degradation of ILs has been reported [71-94], their stability has normally been overestimated due to the use of heating rates above 10 K \cdot min⁻¹. Considering the importance of long-term thermal stability in industrial applications, it is essential to obtain reliable data to evaluate the feasibility of employing a specific IL in each application [95-101]. The search for models capable of predicting long-term stability from the typical dynamic thermogravimetric measurements is more efficient (less time-consuming) and allows the lifetimes of ILs to be used in industrial applications to be estimated [71, 95, 102-105].

In this work, three isoconversional methods are proposed in order to obtain kinetic parameters without any assumption regarding the reaction mechanism. This methodology was applied to determine the long-term stability of 8 fatty acid anion-based ionic liquids (FAILs): methyltrioctylammonium hexanoate $[N_{8,8,8,1}][C_{6:0}]$, methyltrioctylammonium octanoate $[N_{8,8,8,1}][C_{8:0}]$, tetrahexylammonium octanoate $[N_{8,8,8,1}][C_{12:0}]$, methyltrioctylammonium palmitate $[N_{8,8,8,1}][C_{16:0}]$, tetrahexylammonium palmitate $[N_{8,8,8,1}][C_{16:0}]$, tetrahexylammonium palmitate $[N_{8,8,8,1}][C_{16:0}]$, tetrahexylammonium palmitate $[N_{8,8,8,1}][C_{16:0}]$, methyltrioctylammonium stearate $[N_{8,8,8,1}][C_{18:0}]$ and methyltrioctylammonium oleate $[N_{8,8,8,1}][C_{18:1}]$. In addition, isothermal experiments were performed in order to compare their results with those of the model-free methods and determine whether the two methodologies are in good agreement. To the best of our knowledge, no studies focusing on model-free methodology with FAILs have been reported in the literature.

2. Experimental

2.1. Chemicals

Eight fatty acid-based ionic liquids (FAILs), Table 1, were synthesized using a salt metathesis reaction according to the methodology described in Battez *et al.* [106]. The details related to their identification

through ¹H and ¹³C NMR (nuclear magnetic resonance) and FTIR (Fourier-transform infrared spectroscopy) analyses can also be found in Battez *et al.* [106], Blanco *et al.* [61] and Sernaglia *et al.* [69]. Methyltrioctylammonium bromide (\geq 97%) and tetrahexylammonium bromide (\geq 99%) ionic liquids were employed as cation precursor. In addition, several natural fatty acids: hexanoic (\geq 98%), octanoic (\geq 98%), lauric (\geq 98%), palmitic (\geq 98%), stearic (\geq 98%) and oleic (\geq 95%) were used as anion precursors. Both cation and anion precursors were supplied by Sigma-Aldrich and employed without any further purification. After the above-mentioned synthesis procedure, a bright orange liquid product was obtained in all cases, with the molar yield ranging from 85–95%. In addition, a Metrohm 899 coulometer Karl Fischer titration was used to determine the water content of the ionic liquids, obtaining values ranging between 1 and 3%. Finally, the nature of the synthesis employed means that traces of halides could also be present in the final product. Fig. 1 shows the chemical structure and acronym of the 8 FAILs.

IUPAC name	Acronym	Molecular weight (g/mol)	Empirical formula
Methyltrioctylammonium hexanoate	$[N_{8,8,8,1}][C_{6:0}]$	483	C31H65NO2
Methyltrioctylammonium octanoate	$[N_{8,8,8,1}][C_{8:0}]$	511	$C_{33}H_{69}NO_2$
Tetrahexylammonium octanoate	$[N_{6,6,6,6}][C_{8:0}]$	496	C32H66NO2
Methyltrioctylammonium laurate	$[N_{8,8,8,1}][C_{12:0}]$	567	C37H77NO2
Methyltrioctylammonium palmitate	$[N_{8,8,8,1}][C_{16:0}]$	623	$C_{41}H_{85}NO_2$
Tetrahexylammonium palmitate	$[N_{6,6,6,6}][C_{16:0}]$	608	$C_{40}H_{82}NO_2$
Methyltrioctylammonium stearate	$[N_{8,8,8,1}][C_{18:0}]$	651	C43H89NO2
Methyltrioctylammonium oleate	$[N_{8,8,8,1}][C_{18:1}]$	649	C43H87NO2

Table 1 Chemical description of the ILs used.

[N6,6,6,6][C8:0]

 $[N_{8,8,8,1}][C_{6:0}]$



[N6,6,6,6][C16:0]



 $[N_{8,8,8,1}][C_{8:0}]$





Fig. 1 Chemical structures and acronyms of the FAILs.

2.2. Thermal analysis

A TA Instruments DSC SDT Q600 Thermogravimetric Analyzer (TGA) & Differential Scanning Calorimeter (DSC) was employed to perform the thermal analysis. In addition, TA Instruments Universal Analysis 2000 version software was employed to analyse the obtained results. This equipment has the ability to operate in both dynamic and isothermal modes. Dynamic tests were performed with 29-31 mg of each FAIL under a dry nitrogen atmosphere (flow of 50 mL/min), using four different heating rates (5, 10, 15 and 20 K·min⁻¹) from 30 to 600 °C. Isothermal experiments were also carried out under this mentioned atmosphere at three different temperatures (100, 150 and 200 °C) for 12 h and at lower temperature (80 °C) for 24 h. Using TGA (thermogravimetric analysis) and DTG (differential thermogravimetry) data, several parameters could be obtained:

- *T*_{onset}: determined as the point of intersection of the starting-mass baseline and the tangent to the TGA curve at the point of maximum slope (°C).
- *T_{endset}*: intersection point of the curve segment after the inflection occurs and the tangent to the TGA curve at the point of maximum slope (°C).
- $T_{10\%}$: temperature equivalent to 10% of mass loss (°C).
- $T_{50\%}$: temperature equivalent to 50% of mass loss (°C).
- *W*_{total loss}: mass loss at the end of the experiment (%).
- *W*_{onset}: mass loss at decomposition onset temperature (%).

2.3. Kinetic modelling

The main recommendations of the ICTAC Kinetics Committee were followed with the aim of evaluating the multi-step thermal decomposition kinetics, as well as the measurement and parametrization of the process rates [96, 97, 107]. The rate in a thermal-decomposition process can be defined through two parameters: temperature (T) and the extent of reaction or conversion (α), Eq. (1).

$$\frac{d\alpha}{dt} = k(T)f(\alpha) \tag{1}$$

In a thermogravimetric (TG) experiment, where the variation of mass versus temperature is obtained, the extent of reaction is calculated using the following Eq. (2) [96, 104, 108, 109]:

$$\alpha = \frac{m_0 - m_t}{m_o - m_e} \tag{2}$$

where: m_0 is the initial mass, m_t is the mass at time t and m_e is the mass at the end of the test. It should be noted that the conversion (α) can vary from 0 (absence of mass loss) to 1 (complete mass loss). The parameter m_e depends on the atmosphere and the type of substance among other factors; a zero value was assumed for this parameter in this study due to the nature of the FAILs.

The temperature dependence of the rate constant, k(T), in Eq. (1) is described by the Arrhenius Eq. (3) [97].

$$k(T) = A \cdot \exp \frac{-E_a}{RT}$$
(3)

where A is the pre-exponential factor, E_a is the activation energy, R is the gas constant and T is the absolute temperature. Merging Eq. (1) and Eq. (3), the Eq. (4) can be obtained:

$$\frac{d\alpha}{dt} = A \cdot \exp \frac{-E_a}{RT} f(\alpha) \tag{4}$$

In this study, kinetic analysis is based on non-isothermal thermogravimetric experiments, so the above expression can be transformed into a non-isothermal rate expression describing reaction rates as a function of temperature at a constant heating rate, β , Eq. (5):

$$\frac{d\alpha}{dT} = \frac{A}{\beta} \cdot \exp \frac{-E_a}{RT} f(\alpha)$$
(5)

Based on the above equation, model-free isoconversional methods allow the estimation of the activation energy as a function of α without choosing the reaction model. Their basic assumption is the isoconversional principle (the reaction rate for a constant α depends only on temperature). There are a variety of isoconversional methods and two different mathematical categories [95, 98, 99, 102, 104, 109-111] can be

distinguished: i) integral, such as Kissinger-Akahira-Sunose (KAS) and Flynn-Wall-Ozawa (FWO) and ii) differential, the Friedman and Kissinger methods being the most common ones. Therefore, three of these abovementioned isoconversional methods are used in this work (Table 2).

Model free methods	Туре	Expression	Ref.
FWO	Integral	$log(\beta) = log\left(\frac{AE}{g(\alpha)}\right) - 2.315 - \frac{0.457E_a}{RT}$	[95, 99, 110, 111]
KAS	Integral	$ln\left(\frac{\beta}{T^2}\right) = ln\left(\frac{AR}{E_{\alpha}g(\alpha)}\right) - \frac{E_{\alpha}}{RT}$	[95, 99, 104, 109, 110]
Friedman	Differential	$ln\left(\frac{d\alpha}{dt}\right)_{\alpha} = ln(Af(\alpha)) - \frac{E_a}{RT}$	[95,110,111]

Table 2 Isoconversional methods employed in this research.

For applying these methods, it is necessary to use at least three different heating rates. It is important to bear in mind what happens in a thermogravimetric experiment in order to choose the appropriate heating rates. The resultant mass loss should be the combination of thermal decomposition and evaporation kinetics occurring simultaneously [71, 80-86]. Considering that both the decomposition and evaporation rates grow exponentially with temperature (although the decomposition rate is more temperature sensitive than the evaporation rate), the utilization of wide temperature ranges and high heating rates leads to a process in which the thermal decomposition should control the overall mass loss [82]. Therefore, the heating rates used in this research are greater than 5 K·min⁻¹ with the with the objective of ensuring that thermal decomposition is the predominant process, making Eq. (1) negligible. Finally, this methodology allows the estimation of the time (t_a) needed to reach a given conversion (α) under an arbitrary isothermal experiment (T_b), Eq. (6):

$$t_{\alpha} = \frac{\int_{0}^{T_{\alpha}} e^{-E_{\alpha}/RT} dT}{\beta e^{-E_{\alpha}/RT_{0}}}$$
(6)

1 **3. Results and discussion**

- 2 3.1. Thermal decomposition
- 3 The TG and DTG graphs of the 8 FAILs are plotted in Figs. 2 and 3, respectively. All studied substances
- 4 show a multi-step degradation mechanism, which can be seen in Fig. 3, where the DTG curves have an
- 5 irregular shape due the overlapping mass loss processes.
- 6



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8 Fig. 2 Full scale TGA for all FAILs obtained under nitrogen atmosphere at a heating rate of 10 K·min⁻¹.



anion. In this particular case, FAILs with shorter chain anions show a more irregular shape in DTG curves.
 This multi-step mechanism may well be related to the increase in the anion-cation electrostatic interaction.
 As the carbon chain increases in length no shoulders are observed in the DTG curve and a single-step model
 dominates the process.



Fig. 3 DTG for all FAILs obtained under nitrogen atmosphere at a heating rate of 10 K min⁻¹.

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8 Therefore, the thermal stability of FAILs here studied is controlled by both the cation and anion, the cation 9 effect being more important, since samples including the $[N_{6,6,6,6}]^+$ cation were the most thermally unstable. 10 Table 3 shows several parameters obtained from TG plots, such as: T_{onset} , T_{endset} , $T_{10\%}$, $T_{50\%}$, $W_{total loss}$ and 11 W_{onset} . Most of the samples have an onset decomposition temperature (T_{onset}) below 200 °C, with 12 $[N_{8,8,8,1}][C_{16:0}]$, $[N_{8,8,8,1}][C_{18:0}]$ and $[N_{8,8,8,1}][C_{18:1}]$ registering the best values with respect to this parameter, 13 probably due to the slight influence of their longer alkyl chains in the anions [102, 109].

Table 3 Thermal results from dynamic scans obtained under nitrogen atmosphere at 10 K min⁻¹.

FAILs	T_{onset} (°C)	<i>T10%</i> (°C)	<i>T50%</i> (°C)	Tendset (°C)	W _{total} loss (%)	Wonset (%)
$[N_{8,8,8,1}][C_{6:0}]$	190	184	222	262	99.56	10.52
$[N_{8,8,8,1}][C_{8:0}]$	177	178	227	274	99.70	9.68
$[N_{8,8,8,1}][C_{12:0}]$	182	192	232	280	99.82	9.67
$[N_{8,8,8,1}][C_{16:0}]$	200	190	249	290	99.44	13.88
$[N_{8,8,8,1}][C_{18:0}]$	199	190	250	293	100.00	12.44
$[N_{8,8,8,1}][C_{18:1}]$	200	186	252	292	98.61	13.49
$[N_{6,6,6,6}][C_{8:0}]$	177	172	206	232	99.62	14.06
$[N_{6,6,6,6}][C_{16:0}]$	187	176	220	256	99.34	15.17

The same trend is also observed with T_{endset} , $T_{10\%}$ and $T_{50\%}$ parameters. In addition, mass loss of almost 100% has been detected for all samples at the end of the experiment. In view of all these thermal parameters, the sample $[N_{6,6,6,6}][C_{8:0}]$ has the lowest thermal stability. In addition, all the FAILs here studied exhibited lower thermal stability under a nitrogen atmosphere than the traditional ILs tested previously in lubrication studies [102, 104, 105, 109], particularly when compared to those containing the $[NTf_2]^-$ anion.

8

9 3.2. Kinetic analysis

10 Fig. 4 shows different TG plots obtained with four heating rates (5, 10, 15 and 20 K·min⁻¹). This is 11 mandatory for the application of the different model-free kinetics methods because at least three dynamic 12 curves with different heating rates are required. These methods are in agreement with the isoconversional 13 principle which states that the reaction rate at a constant extent of conversion is dependent only on the 14 temperature. This implies that curves plotted at different heating rates cannot intersect if the model is to be 15 considered valid, at least in the conversion range over which activation energy (E_a) remained constant [97, 16 104, 109, 117]. In addition, thermal stability was lower with decreasing values of β for the eight FAILs 17 here studied. This is possibly related to the higher sensitivity of this decomposition reaction at lower heating 18 rates, which agrees with Kok et al. [118]. In addition, it seems that the thermal stability at the lowest heating 19 rate (5 K·min⁻¹) differs from that under the remaining heating rates (10, 15 and 20 K·min⁻¹), especially for 20 the FAILs $[N_{8,8,8,1}][C_{6:0}]$, $[N_{8,8,8,1}][C_{8:0}]$ and $[N_{8,8,8,1}][C_{12:0}]$. This may be because the shorter alkyl chains of 21 these FAILs facilitate the decomposition reaction. Another possible explanation for this result could be 22 that at the lowest heating rate (5 $K \cdot min^{-1}$), the contribution of evaporation to the overall rate of mass loss 23 is not entirely negligible [71].

1 The fits corresponding to the application of the three selected isoconversional methods to the dynamic TG 2 data for all the studied FAILs exhibit good linearity, with $R^2 \ge 0.90$ being obtained in all cases. This 3 isoconversional methodology was applied in all cases for fourteen α values between 1 and 99%. Constant 4 activation energy values should be expected in the case of a single-step reaction. In this case, the activation 5 energy remained practically constant only when the α values were in the range 30-60% (see Table 4), 6 probably due to the complexity of the thermal process. In order to determine the apparent degradation 7 activation energies, calculations using TG and DTG dynamic data must be performed: $\ln (d\alpha/dt)$ 8 (Friedman), $\ln (\beta/T)$ (KAS) and $\log \beta$ (FWO) against 1/T were respectively plotted.





- 1 The apparent activation energy, obtained as the slope of the fitting equation of each isoconversional method, 2 and for each conversion degree, is presented in Table 4. In view of the results, the activation energy values 3 calculated from the three dynamic methods are quite similar, being slightly higher in most cases for KAS 4 and FWO methodologies.
- 5 6

Table 4 Apparent activation energy (KJ/mol) as a function of conversion (30-60%) derived from

E A IL .	M - 41 1 -	Conversion, α (%)				
FAILS	Methods	30	40	50	60	
	KAS	87.43	89.41	88.88	83.04	
$[N_{8,8,8,1}][C_{6:0}]$	FWO	90.50	92.49	90.5	86.69	
	Friedman	85.49	97.35	78.23	70.49	
	KAS	90.81	90.44	87.87	83.91	
$[N_{8,8,8,1}][C_{8:0}]$	FWO	93.85	93.67	91.38	87.77	
	Friedman	97.21	88.12	82.66	75.54	
	KAS	88.17	87.57	84.95	86.82	
$[N_{8,8,8,1}][C_{12:0}]$	FWO	83.84	77.67	75.95	75.32	
	Friedman	66.10	65.82	70.61	71.55	
	KAS	67.26	69.27	71.77	72.19	
$[N_{8,8,8,1}][C_{16:0}]$	FWO	71.84	73.93	76.46	77.01	
	Friedman	68.39	77.04	78.29	72.3	
	KAS	67.22	65.10	63.42	62.97	
$[N_{8,8,8,1}][C_{18:0}]$	FWO	71.85	70.01	68.58	68.3	
	Friedman	78.98	72.25	57.69	63.84	
	KAS	70.62	67.28	63.94	66.50	
$[N_{8,8,8,1}][C_{18:1}]$	FWO	75.01	72.02	71.15	71.59	
	Friedman	61.44	63.52	66.74	71.31	
	KAS	73.77	78.04	76.83	71.93	
$[N_{6,6,6,6}][C_{8:0}]$	FWO	77.47	81.62	80.56	75.99	
	Friedman	81.31	81.43	69.23	50.44	
	KAS	56.71	55.12	51.41	48.92	
$[N_{6,6,6,6}][C_{16:0}]$	FWO	61.52	60.15	56.75	54.51	
	Friedman	53.51	44.46	38.64	43.58	

experiments with heating rates of 5, 10, 15 and 20 K·min⁻¹.

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8 Average values of activation energy were obtained as the mean values of those corresponding to the 9 different conversion values between 30-60% for each isoconversional method, and results are shown in 10 Table 5. In addition, the resultant E_a is calculated as the average value of KAS, FWO and Friedman results, 11 and its uncertainty as a weighted average of the uncertainties associated with each model, where the weight 12 of each model has been inversely proportional to its variance. Finally, the dispersion between models is 13 showed through the variance in the last column. These results indicate that the activation energy values are 1 quite similar, regardless of the methodology, especially in the case of the KAS and FWO methods. 2 Furthermore, the error does not exceed the 10% range in most cases. Analysing the observed trend, the two 3 samples with cation $[N_{6,6,6,6}]^+$ present the lowest E_a mean values. 4 On the other hand, there seem to be higher E_a values in the group of samples containing the anions with the 5 shortest chain length and the same cation $[N_{8,8,8,1}][C_{6:0}] < [N_{8,8,8,1}][C_{8:0}]$ versus the samples with longer 6 anion chain length : $[N_{8,8,8,1}][C_{12:0}] \gg [N_{8,8,8,1}][C_{16:0}] \gg [N_{8,8,8,1}][C_{18:0}] = [N_{8,8,8,1}][C_{18:1}]$, in which the 7 thermal stability decreases with the anion chain length. A parallel difference in behaviour between the two 8 groups has already been reported for another physical property, namely surface tension, by Blanco et al.

9 [61]. These results strongly suggest that the thermal degradation mechanism depends on the alkyl chain

10 length of the anion, the electrostatic force being stronger for [N_{8,8,8,1}][C_{6:0}] and [N_{8,8,8,1}][C_{8:0}].

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Table 5 Average activation energy (kJ/mol) from different models.

		Dispersion			
FAILs	KAS	FWO	Friedman	Average	Models (variance)
$[N_{8,8,8,1}][C_{6:0}]$	87±3	90±3	82±8	87±3	16
$[N_{8,8,8,1}][C_{8:0}]$	$88~{\pm}4$	92±3	83±9	88±4	20
$[N_{8,8,8,1}][C_{12:0}]$	87±2	78±4	69±3	78±2	81
$[N_{8,8,8,1}][C_{16:0}]$	$70\pm\!\!3$	75±3	74±5	73±3	7
$[N_{8,8,8,1}][C_{18:0}]$	65±2	70±2	63±4	66±2	13
$[N_{8,8,8,1}][C_{18:1}]$	67±3	72±2	66±5	68±3	10
$[N_{6,6,6,6}][C_{8:0}]$	75±3	79±3	71±15	75±3	16
$[N_{6,6,6,6}][C_{16:0}]$	53±4	58±4	45±7	52±4	43

12

13 *3.3. Isothermal analysis*

14 In order to complete the thermal study [95, 104, 109], certain isothermal tests were conducted for some 15 FAILs: [N_{8,8,8,1}][C_{6:0}], [N_{8,8,8,1}][C_{12:0}], [N_{6,6,6,6}][C_{16:0}], and [N_{8,8,8,1}][C_{18:1}] under an inert atmosphere. Taking 16 into account the obtained results (Fig. 5), all FAIL samples were almost totally decomposed (conversion 17 values above 90%) after 600 min of testing at 150 °C. Meanwhile, the 4 FAILs were totally decomposed at 18 200 °C when half of the experiment had been performed, with [N_{8,8,8,1}][C_{12:0}] and [N_{6,6,6,6}][C_{16:0}] being 19 completely decomposed in less than 100 min. These results proved that FAILs in the isothermal 20 experiments showed appreciable decomposition at temperatures significantly lower than the values 21 indicated by the Tonset calculated from TGA results. Although all samples are fairly stable at 100 °C under 22 a nitrogen atmosphere and 12 h testing, a new isothermal test was conducted for 24 h at 80 °C with the aim 23 of confirming the previous results. Comparing the results, the isothermal tests are in agreement with the

1 results from the dynamic tests. The influence of the cation was confirmed, tetrahexylammonium palmitate

2 ([N_{6,6,6,6}][C_{16:0}]) being the FAIL that presents the greatest decomposition under the isothermal test at 100

3 °С.



5 Fig. 5 Isothermal scans under nitrogen atmosphere: (O) 80 °C, (\Box) 100 °C, (\bigstar) 150 °C and (×) 200 °C.

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7 3.4. Isoconversional modelling

8 The activation energy (E_a) , conversion (α) and decomposition time (t_a) were estimated as a function of an 9 arbitrary temperature (T_{θ}) by different model-free kinetics methodologies using TGA experimental data 10 under a nitrogen atmosphere (see Table 4). This implies using Eq. (6) with non-isothermal kinetic data in 11 order to predict the FAIL behaviour under isothermal conditions at that temperature (T_0) . It is important to 12 bear in mind that this arbitrary temperature (T_0) should not be far away from the experimental temperature 13 (T_{α}) over the range of T_{α} in which the E_{α} remained practically constant, in order to avoid significant relative 14 errors [119]. Therefore, the thermal stability of ionic liquids could be estimated by using short-term non-15 isothermal thermogravimetric measurements at different heating rates with the objective of applying a 16 kinetic model and obtaining kinetic parameters. In order to solve the mentioned equation, the integral is 17 approximated using the equation proposed by Wanjun et al. [120]. Finally, the necessary time at which

1 each conversion value is reached at a given temperature ($T_0 = 200$ °C) was estimated [104, 109, 121, 122]



2 and the results are shown in Fig. 6.





1 Analysing the obtained results, the 50% conversion mark at 100 °C is obtained in less than 300 min with 2 $[N_{6,6,6,6}][C_{16:0}]$, whereas $[N_{8,8,8,1}][C_{12:0}]$ and $[N_{8,8,8,1}][C_{18:1}]$ needed around 1500 and 2400 min, respectively. 3 On the other hand, the $[N_{8,8,8,1}][C_{6:0}]$ is the most thermally stable FAIL from a long-term thermal stability 4 point of view, reaching the 50% conversion mark at 100 °C after more than 3500 min. The thermal stability 5 trend is slightly modified at increasing temperature. This implies that [N_{6,6,6,6}][C_{16:0}] remains the least stable 6 FAIL, reaching the 50 % conversion mark in 22 min at 150 °C, confirming the cation effect as the most 7 important factor influencing thermal decomposition. However, [N_{8,8,8,1}][C_{18:1}] is now the most thermally 8 stable FAIL at this temperature, needing around 150 min to reach the mentioned conversion compared to 9 102 and 72 min for $[N_{8,8,8,1}]$ [C6:0] and $[N_{8,8,8,1}]$ [C12:0], respectively. It seems that the temperature increase 10 implies that less effort is necessary to overcome the anion-cation electrostatic interaction, which possibly 11 causes a trend of thermal stability proportional to the chain length of the anion. Finally, results seen in the 12 dynamic and isothermal tests are clearly supported by the isoconversional methodology: the cation effect 13 is very pronounced, the $[N_{6,6,6,6}][C_{16:0}]$ being the FAIL that takes the least time to reach each one of the 14 conversion values shown in Fig. 6. 15 In addition, the comparison between isothermal (experimental) and isoconversional (model free method) 16 values at $T_0 = 200$ °C (Fig. 7) were carried out for some of the FAILs: $[N_{8,8,8,1}][C_{6:0}]$, $[N_{8,8,8,1}][C_{12:0}]$, 17 $[N_{6,6,6,6}][C_{16:0}]$ and $[N_{8,8,8,1}][C_{18:1}]$ under a nitrogen atmosphere. From the results shown in Fig. 7, it is 18 possible to estimate the time required for a conversion of the studied sample at a given temperature. The 19 best fit between experimental and model results are for the $[N_{8,8,8,1}][C_{12:0}]$ sample. The experimental results 20 at 200 °C indicate that thermal decomposition reached 30, 40, 50 and 60% conversion at 5, 8, 11 and 16 21 min, respectively, and the calculated values were 3, 5, 7 and 11 min, respectively. Therefore, the results

22 from models showed good agreement. For the other samples, there is also a good level of agreement,

especially at lower conversion values, as can be seen in Fig 7.





3

4

Fig. 7 Comparison between experimental and model results for $[N_{8.8.8.1}][C_{12:0}]$, $[N_{8,8,8,1}][C_{6:0}]$, $[N_{6,6,6,6}][C_{16:0}]$ and $[N_{8,8,8,1}][C_{18:1}]$ at $T_0 = 200$ °C.

5 4. Conclusions

6 The thermal degradation of eight novel fatty acid anion-based ILs (FAILs): methyltrioctylammonium 7 hexanoate $[N_{8,8,8,1}][C_{6:0}]$, methyltrioctylammonium octanoate $[N_{8,8,8,1}][C_{8:0}]$, tetrahexylammonium 8 octanoate $[N_{6,6,6,6}][C_{8:0}]$, methyltrioctylammonium laurate $[N_{8,8,8,1}][C_{12:0}]$, methyltrioctylammonium 9 palmitate $[N_{8,8,8,1}][C_{16:0}]$, tetrahexylammonium palmitate $[N_{6,6,6,6}][C_{16:0}]$, methyltrioctylammonium stearate 10 $[N_{8,8,8,1}][C_{18:0}]$ and methyltrioctylammonium oleate $[N_{8,8,8,1}][C_{18:1}]$, was studied under a nitrogen 11 atmosphere using both dynamic and isothermal approaches. The main conclusions extracted from the 12 obtained results are the following:

The thermal stability of these FAILs is controlled by both the cation and anion, the cation effect
 being more important since samples including the [N_{6,6,6,6}]⁺ cation were the most thermally
 unstable.

1	٠	Most samples have a decomposition onset temperature (T_{onset}) below 200 °C and the
2		$[N_{8,8,8,1}][C_{16:0}]$, $[N_{8,8,8,1}][C_{18:0}]$ and $[N_{8,8,8,1}][C_{18:1}]$ had the higher T_{onset} values, probably due to the
3		longer alkyl chain length in the anion.
4	•	All the FAILs exhibited lower thermal stability under a nitrogen atmosphere than commercially
5		available ILs tested before in lubrication studies, especially those containing the $[NTf_2]^-$ anion.
6	•	FAILs in isothermal experiments showed appreciable decomposition at temperatures significantly
7		lower than the values indicated by the T_{onset} calculated from dynamic TGA.
8	•	The [N _{8,8,8,1}][C _{6:0}] and [N _{8,8,8,1}][C _{8:0}] showed the highest long-term thermal stability, probably
9		related to their stronger anion-cation electrostatic interaction. This led to the multi-step thermal
10		decomposition mechanism observed in the DTG results.
11	•	The experimental isothermal results for the [N _{8,8,8,1}][C _{12:0}] sample agree with the model-free
12		methods.
13		

5. Nomenclature

A	$(m^3 \cdot mol^{-1})^{n-1}s^{-1}$	Pre-exponential factor
Ea	kJ/mol	Activation Energy
М	mol	Molar mass of the ionic liquid
$f(\alpha), g(\alpha)$	-	Reaction models
<i>k(T)</i>	J/K	Temperature dependent constant
R	J/K/mol	Gas constant
t	S	Time
Τ	°C	Temperature
Tonset	°C	Onset Temperature
Tendset	°C	Endset Temperature
<i>T</i> 10%	°C	Temperature at 10% of mass loss
<i>T</i> 50%	°C	Temperature at 50% of mass loss
Tθ	°C	Arbitrary temperature to a given extent of reaction, α
<i>M</i> _i	kg	Initial mass
Me	kg	Mass at the end of the experiment
m_t	kg	Mass at time, t

	W total loss	%	Total weight loss
	Wonset	%	Weight loss at Tonset
	α	-	Extent of reaction
	β	K · min ⁻¹	Heating rate
1			
2			
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9			
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