

1 **ELECTROCHEMICAL DEGRADATION OF NAPROXEN FROM WATER BY ANODIC**
2 **OXIDATION WITH MULTIWALL CARBON NANOTUBES GLASSY CARBON ELECTRODE**

3
4 **Short tittle: ELECTROCHEMICAL OXIDATION OF NAPROXEN BY CARBON**
5 **NANOTUBES AT CONSTANT POTENTIAL**

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10 **Abstract**

11 Naproxen (NPX) degradation was investigated by anodic oxidation both at constant potential
12 and by cyclic voltammetry (CV), using this last technique for optimizing reaction conditions and
13 catalyst properties. Three MWCNTs-promoted electrodes were used (MWCNT, MWCNT-COOH
14 and MWCNT-NH₂) and a two steps oxidation process was observed in all the cases. At the
15 optimized conditions (volume of MWCNT = 15 μL), the influence of the scan rate indicates the
16 diffusion – adsorption control of the process. Likewise, the kinetic study of NPX degradation at
17 fix potential, considering two different stirring speeds (250 and 500 rpm), indicates that
18 degradation rate increases with the stirring speed. After 20 h, NPX is degraded even an 82.5 %,
19 whereas the mineralization reaches almost 70 % as it was obtained from TOC analysis.
20 pH effect was also analysed, in the range 5-11, observing a positive effect at low pH.
21 Concerning the surface chemistry of the electrode, MWCNT-NH₂, with the highest isoelectric
22 point (4.70), is the most promising material due to the improved interactions with the
23 reactant. From these observations, a pathway is proposed, which includes two steps of
24 electrochemical oxidation followed by subsequent oxidation steps, until mineralization of the
25 NPX, attributed mainly to active chlorine species and ·OH.

26
27 **Keywords:** anodic oxidation, degradation pathway, functionalization, multiwall carbon
28 nanotubes, Naproxen

29 INTRODUCTION

30 Nonsteroidal anti-inflammatory drugs (NSAIDs), belonging to pharmaceuticals and personal
31 care products (PPCPs), are widely used for the treatment of headaches, arthritis, spondylitis,
32 etc. and even in cancer treatments (Wojcieszńska *et al.* 2014; Coria *et al.* 2016). In addition,
33 many of them are non-prescription drugs being more accessible, thus, their consumption is of
34 several tons per year in developed countries (Loss *et al.* 2013; Wojcieszńska *et al.* 2014).

35 Among NSAIDs, Naproxen (NPX) is one of the most commonly used (Ding *et al.* 2017).

36 Because of the increasing consumption of NSAIDs, direct disposal of these compounds into
37 aquatic systems has increased their presence in rivers and groundwater. NSAIDs are polar, so
38 soluble in water, and its removal efficiency in wastewater treatment plants (WWTP) is just
39 around 20% (Coria *et al.* 2016). Concretely, in the case of Naproxen (NPX), the removal
40 efficiency in WWTP reaches values lower than 15%.

41 Loss *et al.* (2013) found the NPX presence in 69 of the 100 studied European rivers, from 27
42 different countries, in concentrations higher than $2.027 \text{ ng}\cdot\text{L}^{-1}$. Although, NSAIDs concentration
43 is usually low in water ($\text{ng}\cdot\text{L}^{-1}$ or $\mu\text{g}\cdot\text{L}^{-1}$), the continuous exposure to these compounds may
44 have adverse effects on living organisms; gastrointestinal and renal effects were described for
45 NPX (Ding *et al.* 2017).

46 The most studied methods of removing NPX from water and wastewater are: adsorption
47 (Katsigiannis *et al.* 2015), biodegradation (Wojcieszńska *et al.* 2014; Ding *et al.* 2017) and
48 photodegradation (Štrbac *et al.* 2018). In the case of adsorption, removal efficiency values
49 from 50 to 100% can be obtained depending on the adsorbent. For example, adsorption onto
50 granular activated carbon removes 65.6% of NPX (Katsigiannis *et al.* 2015). The main drawback
51 of the adsorption is the pollutant transference from the liquid to a solid phase (adsorbent), so
52 a further treatment for the pollutant removal is necessary (Chin *et al.* 2014). Biodegradation
53 techniques present the inconvenience of the long time needed for an effective degradation,
54 reaching even several days (Ding *et al.* 2017). Photodegradation techniques have

55 demonstrated to be an effective way to degrade these kind of pollutants, with removal
56 efficiencies close to 90% for ozonation, or around 100% for photolysis. Nevertheless, the
57 byproducts are usually found to be more toxic than the parent compounds.

58 In the search for a green-technology for NPX removal, the electrochemical oxidation is an
59 interesting alternative, since in the mineralization of the pollutants, it does not use any
60 external oxidizing agent. The only requirement is the suitable electrode to achieve the
61 pollutant oxidation (Chin *et al.* 2014).

62 In this way, chemically modified electrodes have been used to boost the electron transfer for
63 the electro-oxidation of organic pollutants (Ardelean *et al.* 2016). Both carbon nanotubes
64 (CNTs) and multiwall carbon nanotubes (MWCNTs), have been widely used to improve
65 electrode performance because of their exceptional features: high electrical conduction, high
66 surface area, chemical stability and good hydrophobicity. Carbon nanotubes present several
67 advantages; they produce a decrease in the overpotential of electrochemical oxidation
68 reactions, as well as an increase in the electrode active surface area, and provide greater
69 electrode stability.

70 The performance of three kinds of MWCNT (non- functionalized (MWCNT), functionalized with
71 carboxylic (MWCNT-COOH) and amine (MWCNT-NH₂) groups) for the electrochemical
72 degradation of NPX was studied in this work. These materials were already used in the
73 electrochemical oxidation of both NAL and MPET, using cyclic voltammetry for optimizing the
74 operation conditions (Patiño *et al.* 2017; Patiño *et al.* 2018). This technique allows a systematic
75 study of the electrochemical oxidation, as well as identifying the effect of both electrode
76 properties and operation conditions. However, the novelty of this work is double, on one side,
77 the use of Naproxen as reactant and the study of the influence of both the pH, and the
78 functionalization of the MWCNTs surface; and on the other hand, the effect of the stirring
79 speed on the degradation of NPX.

80 Naproxen electrochemical degradation by cyclic voltammetry was already study by Chin (2014)
81 with platinum nanoparticles supported both on fluorine tin oxide (FTO) and MWCNTs/FTO,
82 thus the study was focused on the role of Pt. Likewise, naproxen detection by CV using
83 MWCNTs modified electrode was researched (Montes *et al.* 2016). Taskhourian (2014) studied
84 the effect of the incorporation of both, ZnO nanoparticles and MWCNTs in the electrode for
85 the NPX electrooxidation. Thus, a deep study of the MWCNTs and its functionalization on the
86 NPX removal is, to the best of our knowledge, unexplored. What is more, the role of the
87 functionalization and the influence of pH for each functional group is addressed here for the
88 first time. Furthermore, this work studies the influence of stirring speed, proposing a kinetic
89 and a degradation pathway based on the detected by-products.

90

91 **MATERIALS AND METHODS**

92 **Reagents and materials**

93 Naproxen (NPX) was purchased from Sigma-Aldrich with a purity $\geq 98\%$. All reactants used in
94 the buffer solutions were from Sigma-Aldrich and in analytical grade. Phosphate buffer (PBS)
95 solutions were prepared by mixing the corresponding amount of sodium chloride (NaCl),
96 potassium chloride (KCl), potassium phosphate monobasic (KH_2PO_4) and sodium phosphate
97 dibasic (Na_2HPO_4).
98 Three different MWCNT manufactured by DropSense have been checked: non-functionalized
99 MWCNT, MWCNT functionalized with -COOH groups (MWCNT-COOH) and with -NH₂ groups
100 (MWCNT-NH₂), whose main properties were determined in previous works (Patiño *et al.* 2017;
101 Patiño *et al.* 2018).

102 **Preparation of the different MWCNT modified GCEs.**

103 GCE electrodes were modified following the procedure optimized in our previous work (Patiño
104 *et al.* 2017). GCE was polished with aluminium slurry and rinsed with distilled water prior to
105 their modification. After drying at room temperature, different volumes (5-20 μL) of a MWCNT

106 suspension in dimethylformamide (DMF) (concentration of $0.25 \text{ g}\cdot\text{L}^{-1}$) were deposited on the
107 electrode surface and dried at room temperature before electrochemical test.

108 **Electrochemical measurements and analytical instrument**

109 Cyclic voltammograms were performed using a Zahner XPOT Potentiostat in order to
110 characterize the system, step prior to the degradation study, since it allows an optimization of
111 the variables that affect the degradation. A conventional three electrode cell was used with
112 bare or modified glassy carbon electrodes (GCE) as working electrode, saturated calomel (SCE)
113 as reference electrode and platinum (Pt) as auxiliary electrode.

114 Degradation test were carried out at constant potential, using MWCNT-GCE as anode and
115 platinum electrode as cathode. In all cases, the solution was deoxygenated before each
116 measurement in order to prevent any oxygen interferences in the obtained signals.

117 NPX samples obtained in the degradation tests were analysed and quantified by High Pressure
118 Liquid Chromatography (HPLC) using an Agilent 1200 with an UV-VIS detector and a 150 mm
119 Zorbax SB-Aq column. The reaction products obtained were determined by high performance
120 liquid chromatography with mass spectrometry detector (LC-MS), using a UPLC Agilent
121 6460.2.3. NPX degradation was confirmed by total organic carbon (TOC) measurements, which
122 were carried out using a TOC analyser (Shimadzu TOC-VCSH).

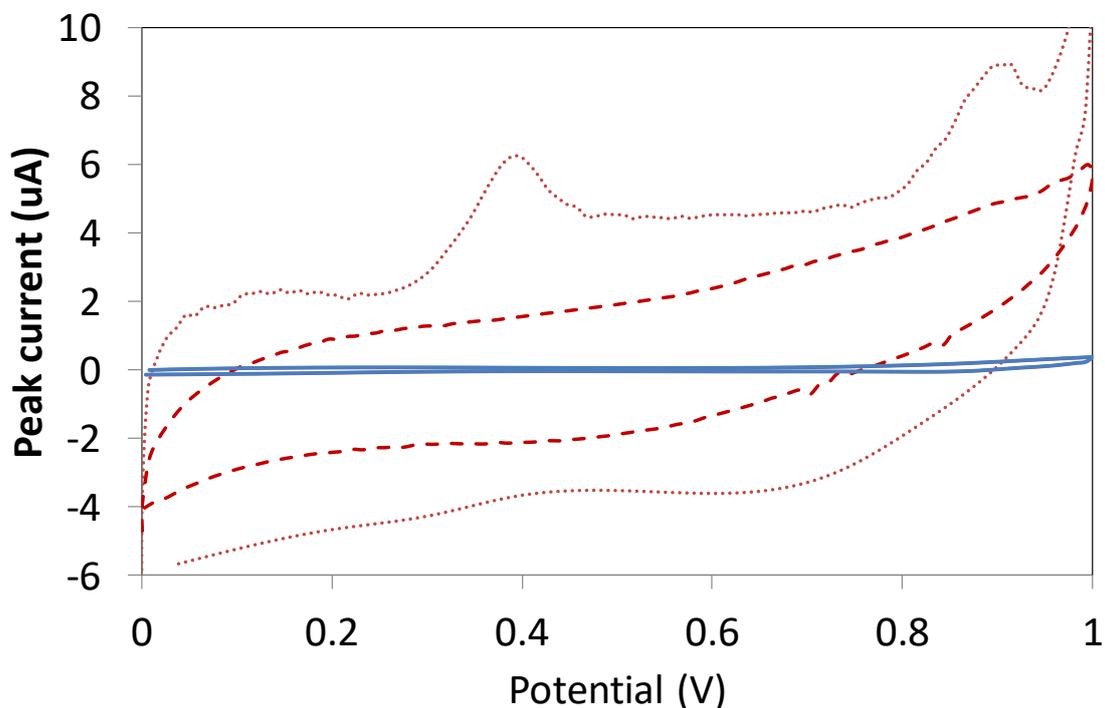
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124 **RESULTS AND DISCUSSION**

125 **Voltammetric naproxen oxidation on MWCNT-GCE and bare electrode**

126 Figure 1 shows the CV obtained for the naproxen oxidation at MWCNT-GCE, in 19 ppm
127 naproxen and PBS buffer of pH = 7.5 at the scan rate of 50 mV/s and with a stirring speed of
128 500 rpm. Two irreversible oxidation peaks were observed at 0.35 and 0.88 V. In a previous
129 essay on the bare-GCE no peaks were detected at this concentration (19 ppm), whereas not
130 electrochemical signals were observed in the blank experiment (absence of NPX) on the

131 MWCNT-GCE. Thus, the MWCNT presence improves the electron transfer process and
132 therefore, the naproxen oxidation.



133
134 Figure 1. CVs of bare-GCE and MWCNT-GCE as working electrodes in the presence of 19 ppm of
135 NPX at scan rate of 50 mVs^{-1} , $\text{pH} = 7.5$ and stirring speed of 500 rpm. Bare- GCE (—), MWCNT-
136 GCE blank (- - -) and MWCNT-GCE with NPX (·····).

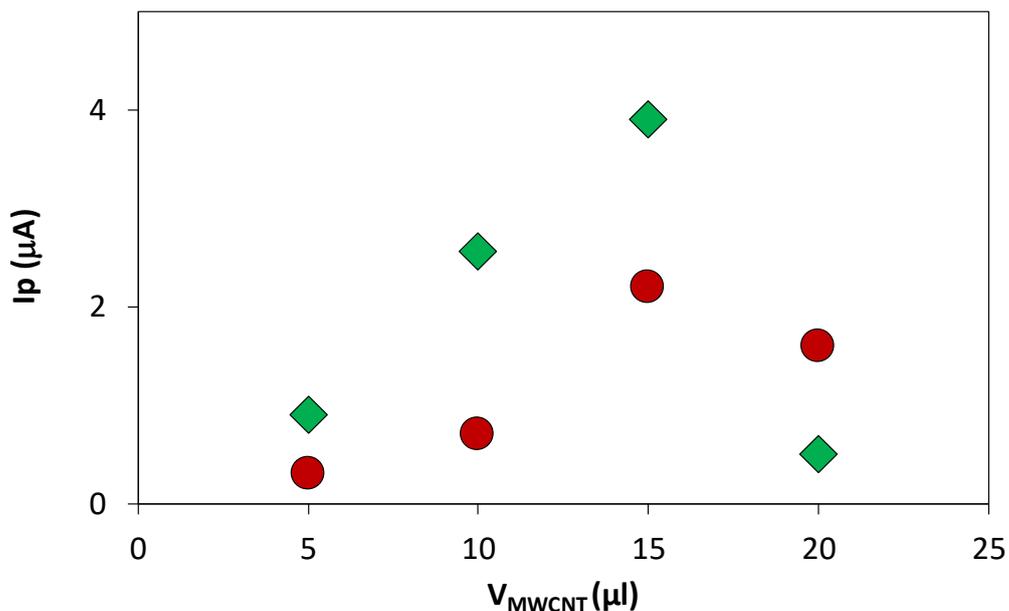
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138 Reported works on electrooxidation of NPX show both a single irreversible oxidation peak for
139 naproxen, and several works have found the existence of two irreversible oxidation peaks. In
140 the first group, Soltani *et al.* (2018) observed a well defined anodic peak at 0.936 V using a
141 carbon paste electrode modified with activated carbon. Tashkhourian (2014) obtained similar
142 results, in this case on ZnO-MWCNTs electrodes, as well as Ardelean (2016) on a BDD
143 electrode, where a peak at a potential of 0.9 V was detected on a CNF epoxy electrode. In the
144 second group, Montes *et al.* (2016) and Aguilar-Lira *et al.* (2015) found two irreversible
145 oxidation peaks between 0.835-1 and 1.131-1.21 V, where the working electrodes were GCE or
146 modified-GCE and graphite; the reference electrodes were Ag/AgCl/saturated KCl and Ag/AgCl,
147 respectively; and Pt and carbon bar were used as auxiliary electrodes, respectively. Likewise,

148 Sarhangzadeh (2015) with MWCNT and graphite hybrid electrodes, using a Pt wire as auxiliary
149 and a saturated calomel electrode (SCE) as reference electrodes, obtained an irreversible
150 oxidation peak at around 0.7 V (pH = 7), and a second reversible peak at about 0.4 V. Thus, it is
151 obvious that add to the working electrode, the choose of both the auxiliary and reference
152 electrodes conditioned the potential, being observed similar potential intervals as in our work
153 in the case of using a saturated calomel (SCE) as reference electrode and a platinum (Pt) as
154 auxiliary electrode. In fact, measurements of different reference electrodes versus each other
155 confirm potential shifts of even 400 mV for the CH₃CN at 25 °C (Pavlishchuk and Addison
156 2000).

157 **Effect of catalyst loading and CV scan rate on NPX oxidation**

158 The effect of the volume of MWCNT to drop on the electrode surface was studied from 5 to 20
159 μL (Figure 2). When the volume was increased from 5 to 15 μL, the peak current also increased
160 due to the increased amount of MWCNT and as consequence, the increased effective surface
161 area. By increasing the effective surface area, the concentration of NPX on the electrode
162 surface increases, favouring its oxidation. On the other hand, when the volume of MWCNT
163 increases up to 20 μL, the peak current decreased. The same behaviour was already observed
164 in previous works (Jain and Sharma 2012; Patiño *et al.* 2017). So, an intermediate film
165 thickness is necessary to allow degradation, but too thick nanotubes layer promote its
166 instability. For this reason, the optimum amount of MWCNT to drop on the electrode surface is
167 15 μL.



168

169 Figure 2. Optimization of the MWCNT volume to drop on the electrode surface. 19 ppm of NPX
 170 in PBS at pH 7.5 ◆ Oxidation peak at 0.33 V, and ● Oxidation peak at 0.88 V

171

172 Scan rate (SR, v) influences the rate of adsorption of species on the electrode. By plotting \log

173 I_p vs $\log v$, the process is assumed to be controlled by adsorption when the slope is close to

174 1.0 and controlled by diffusion if it is close to 0.5. An intermediate slope value indicates that

175 the process is a mixed control: diffusion-adsorption. A linear regression was obtained for both

176 peaks (Figure 3) and the equations can be expressed according to Eq. 1 and Eq. 2.

$$177 \log I_p = 0.6811 \log v - 0.8953 \quad (r^2=0.97) \quad (1)$$

$$178 \log I_p = 0.9949 \log v - 1.7066 \quad (r^2=0.98) \quad (2)$$

179 For the oxidation peak at 0.33 V, the slope of 0.6811 indicates that the process has a mixed

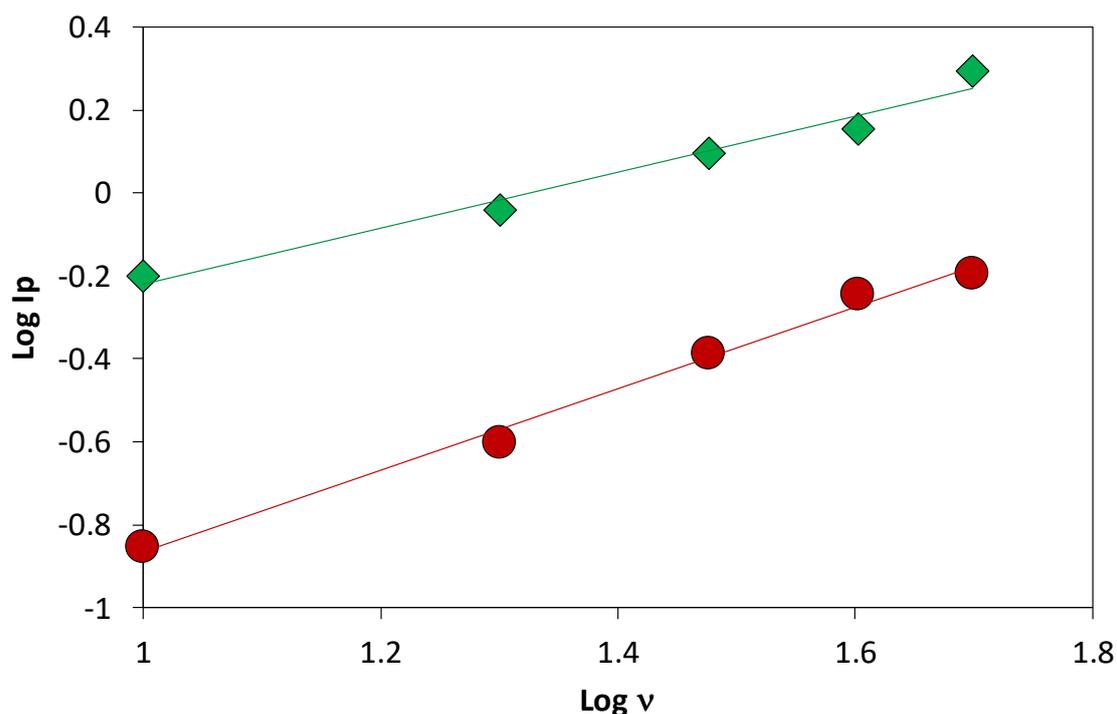
180 control: diffusion-adsorption (Wu *et al.*, 2016). On the other hand, for the oxidation peak at

181 0.88 V, the slope close to 1.0 confirms that the process is controlled by adsorption (Shin *et al.*

182 2011). This fact suggest that the electrochemically relevant process consists of two serial

183 reactions of adsorbed species, the first one being faster and therefore more likely to be

184 controlled by mass transfer.



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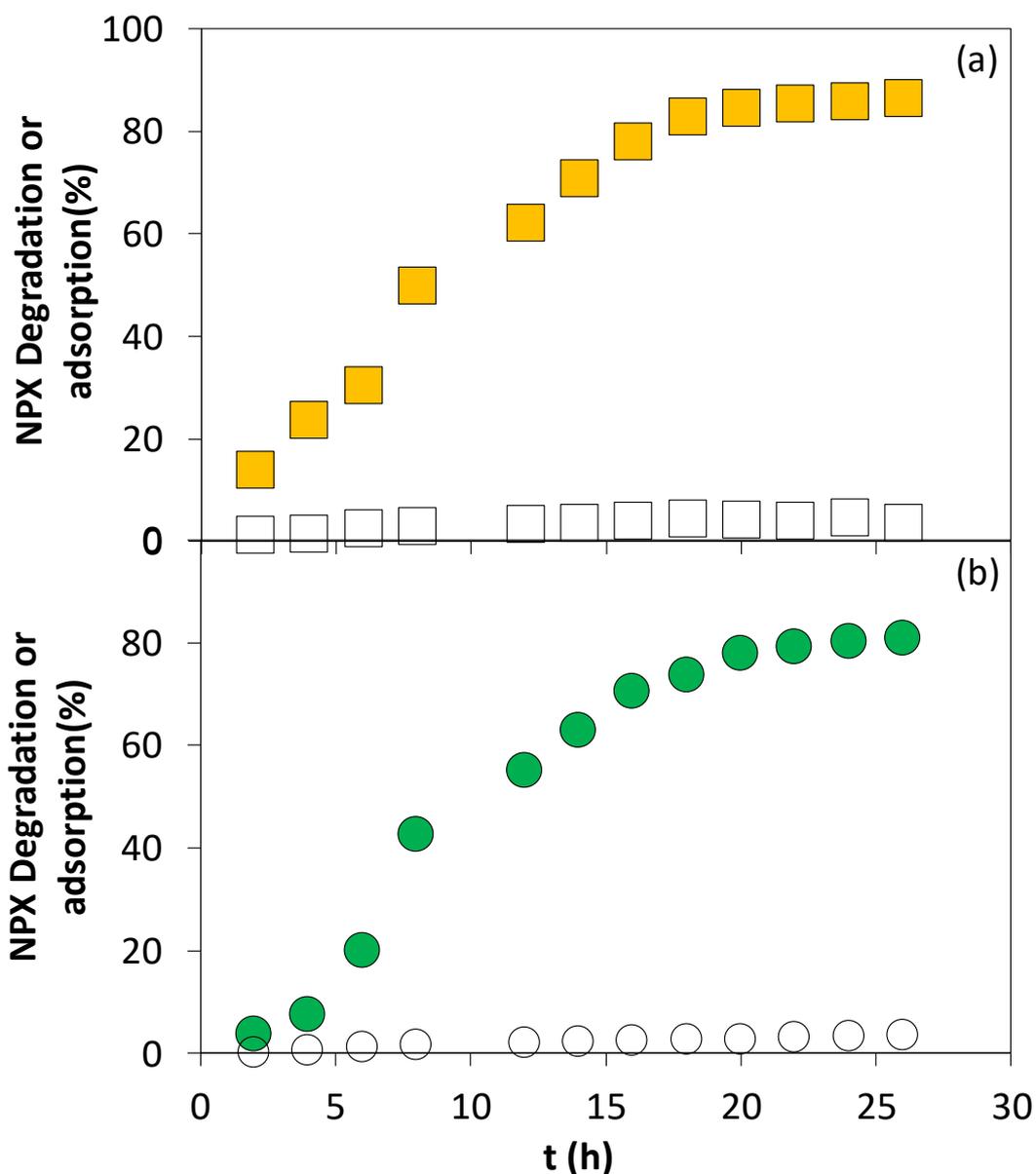
186 Figure 3. log Ip against log v. 19 ppm of NPX in PBS at pH 5.0. ◆ Oxidation peak at 0.33 V, and
 187 ● Oxidation peak at 0.88 V

188

189 **NPX degradation on MWCNTs-GCE in a batch reactor at constant potential**

190 Since the practical application of this process to the treatment of NPX-polluted waters require
 191 the operation at constant potential, the following set of experiments were performed at batch
 192 mode and working at fixed potential.

193 The degradation of NPX using MWCNT-GCE electrode at fixed potential (1.5V) in a batch
 194 reactor, with a total volume of 10 mL and an initial concentration of 19 ppm under stirring at
 195 optimal conditions - pH 7.5 and $V_{\text{MWCNT}}=15 \mu\text{L}$ -, is shown in Figure 4. Likewise, the effect of
 196 stirring speed on the NPX degradation was considered, working at two different stirring
 197 rates, 250 and 500 rpm.



198

199 Figure 4. NPX degradation (filled symbol) and NPX adsorbed on the electrode surface (empty
 200 symbols) at constant potential (+1.5V) with MWCNT-GCE as anode under stirring: 500 rpm (a)
 201 and 250 rpm (b). 19 ppm of NPX in 10 mL of PBS at pH 7.5.

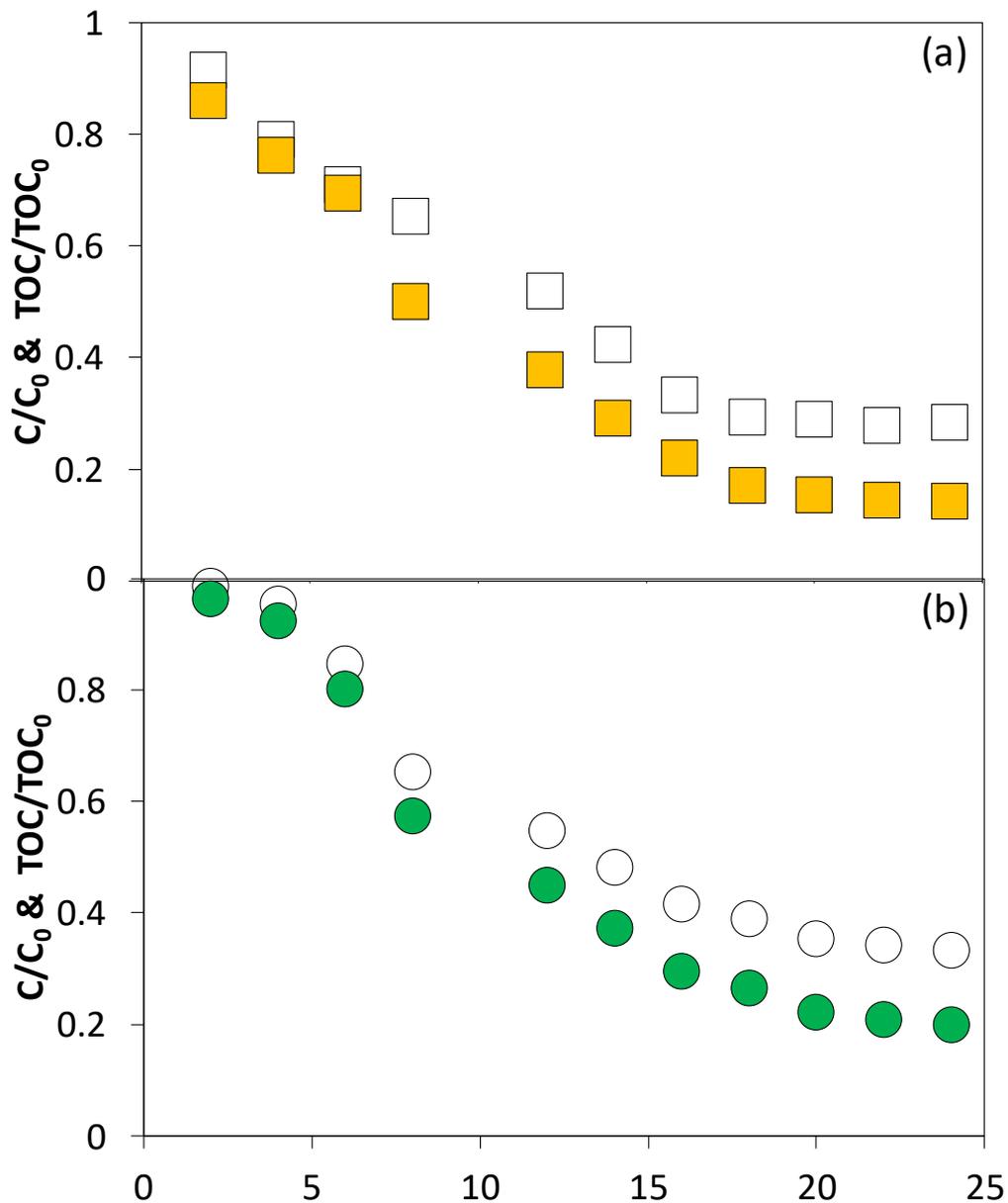
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203 NPX concentration evolution, obtained from HPLC analysis of the NPX solution, reveals that the
 204 maximum NPX removal from the water samples, 86.5%, is reached after 22h at 500 rpm. When
 205 the stirring speed was reduced by half, the removal efficiency was \approx 81%. This fact suggests
 206 that stirring speed does not significantly influence the NPX external and internal diffusion from

207 the solution to electrode surface, as well as its adsorption on it. In both cases, degradation
208 remains constant after 20-22 hours, suggesting saturation of the electrode surface.

209 NPX adsorption on the electrode could mask the actual degradation value, thus the amount of
210 NPX adsorbed on the electrode surface was quantified in an additional experiment without
211 electrochemical reaction. From Figure 4, it is observed that this amount is lower than 4% of the
212 degradation obtained in both cases – 250 and 500 rpm –. Therefore, the maximum NPX
213 degradation would be 82.5% and 77% for 500 and 250 rpm, respectively.

214 From NPX concentration is still unknown the actual decontamination potential of the
215 technique, since organic byproducts in the oxidations could be produced. Hence, the total
216 organic carbon (TOC) evolution is showed in Figure 5, together with the C/C_0 ratio. As can be
217 seen, the NPX disappearance is greater than that of TOC. It is due to the presence of
218 byproducts, that have not been completely mineralized and influence on the TOC results. The
219 residual TOC after 20 h is less than 30% at 500 rpm and close to 33% at 250 rpm, which
220 confirm NPX removal. What is more, considering the unreacted NPX in the solution, just about
221 40 % of the residual TOC corresponds to byproducts of the reaction, which corroborated that
222 TOC does not decrease at the same time than NPX concentration. These results are promising,
223 especially in comparison with those obtained by other techniques. In this way, biological
224 techniques reached a maximum degradation of 80% after 30-35 days (Wojcieszńska *et al.*
225 2014; Ding *et al.* 2017) whereas by photocatalytic ones, total degradation of NPX was observed
226 after half an hour on ZnO and TiO₂ materials (Kanakaraju *et al.* 2015; Štrbac *et al.* 2018).



227

228 Figure 5. C/C_0 evolution (filled symbol) and TOC/TOC_0 evolution (empty symbols) at constant
 229 potential (+1.5V) with MWCNT-GCE as anode under stirring: 500 rpm (a) and 250 rpm (b). 19
 230 ppm of NPX in 10 mL of PBS at pH 7.5.

231

232 The NPX concentration with time was fitted to a pseudo-first order kinetic equation,

233 considering data until electrode saturation, (Eq. 3).

$$234 \quad r_0 = -\frac{dC}{dt} = -k \cdot C \quad (3)$$

235 Where C ($\text{mg}\cdot\text{L}^{-1}$) is the NPX concentration, t is the reaction time (h) and k is the degradation

236 rate constant (h^{-1}).

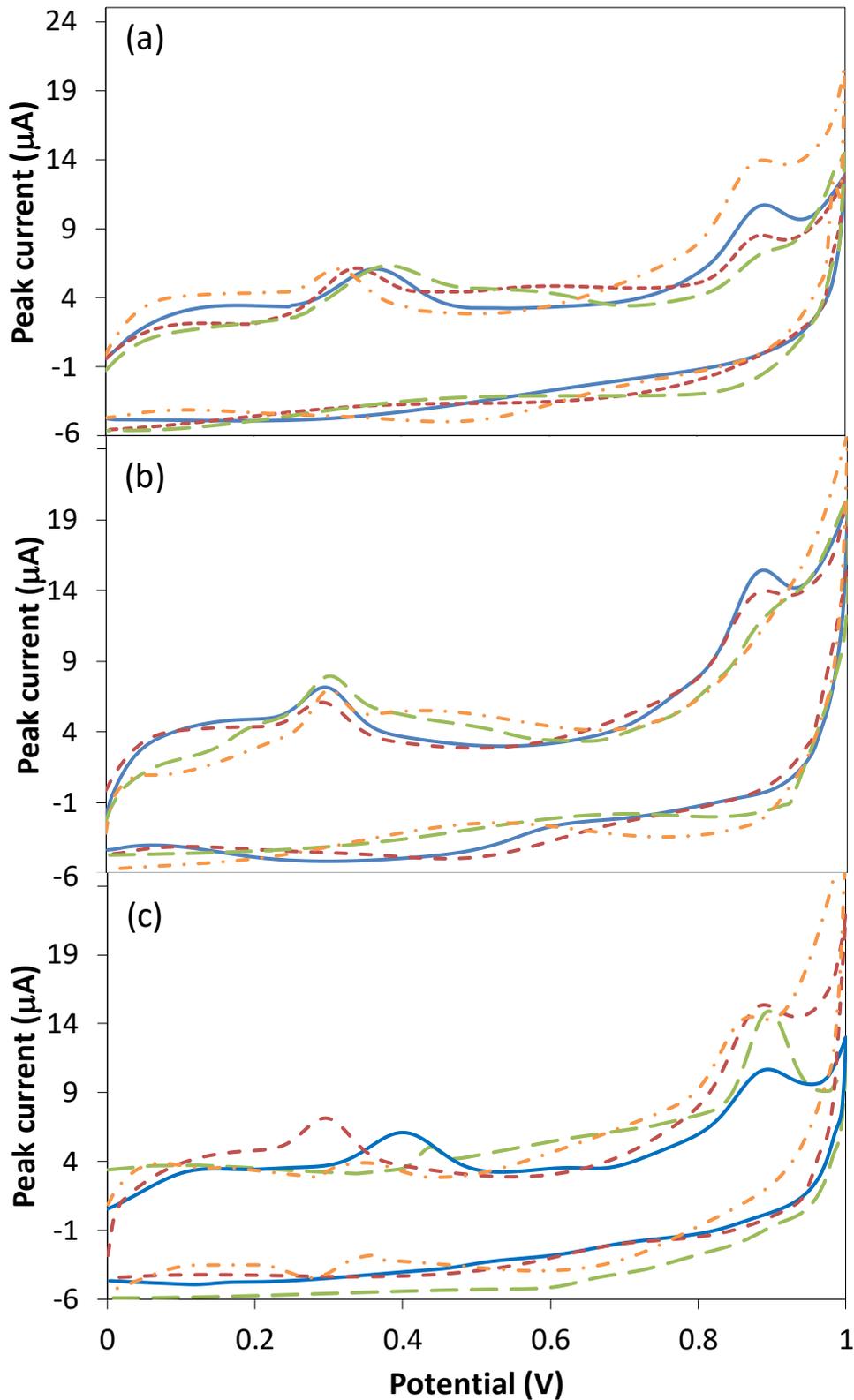
237 The experimental results fit perfectly to the proposed model with a correlation coefficient $r^2=$
238 0.98, obtaining a degradation constant of 0.10 h^{-1} at 500 rpm and 0.08 h at 250 rpm, thus NPX
239 degradation rate increases with the stirring speed. These results are congruent with the
240 diffusion-adsorption control of the process previously stated, since the mass transfer
241 limitations decrease as the stirring velocity increases.

242 **Effect of pH and functionalization of MWCNTs on the naproxen oxidation**

243 In order to get a deep insight into the effect of the surface into the NPX oxidation, it was
244 investigated in the interval of 5-11 (Figure 6). The pH range was selected from the saturated
245 solubility studies of naproxen in aqueous medium of Kumar *et al.* (2015), where it is observed
246 that the drug solubility at pH lower than 5 was very low.

247

248



249

250 Figure 6. CVs in the presence of 19 ppm of NPX in PBS at different pH and scan rate of
 251 50 mVs⁻¹, using as working electrode: (a) MWCNT, (b) MWCNT-NH₂ and (c) MWCNT-
 252 COOH. — pH 5, — pH 7, - - pH 9 and - · - pH 11.

253 From Figure 6a is observed that the oxidation peak potential shifted, when the pH decreases,
254 to lower values in the interval under study (5-11). This effect is observed in both oxidation
255 peaks, with displacements from 0.37 to 0.33 V and from 0.91 to 0.85 V. Concerning the peak
256 current, the low potential peak decreases in the range 5- 11 pH, thus the NPX oxidation
257 increased at the most acidic pH. The same finding was already reached by Chin (2014) for the
258 oxidation of NPX; what is more, in an experiment without pH control, a decrease in the pH
259 with the reaction extension was observed, pointed out the formation of acidic species. In the
260 case of the high potential peak, the more basic medium seems to favour the oxidation process,
261 although this effect is less marked.

262 Considering that the pKa of naproxen is 4.12, the molecule presents in the deprotonated form
263 at all pH considered in this work. Likewise, the isoelectric point of the MWCNT is 4.19, so
264 repulsion forces between the negative charged surface and the reactant could occur (Patiño *et al.*
265 *2015*). These repulsive forces will increase their intensity with the pH, hence the best
266 performance of pH=5.

267 Voltamperograms corresponding to NPX oxidation on MWCNT-NH₂ modified electrode are
268 shown in Figure 6b, whereas the corresponding to MWCNT-COOH are shown in Figure 6c. As
269 in the MWCNT electrode, a shift of the peaks potential towards less positive values with the
270 lower pH is observed by MWCNT-NH₂ electrode, although the intervals are narrower (0.27-0.3
271 V; 0.9-0.87 V). For MWCNT-COOH, the peak potential range is so tight among the different pH
272 that no conclusions could be drawn. The isoelectric points are 4.70 and 0.64 for MWCNT-NH₂
273 and MWCNT-COOH respectively, thus, the repulsive forces between deprotonated reactive
274 molecule and the surface of the MWCNT-COOH could hinder the extension of the reaction,
275 even at the lowest pH (Patiño *et al.* 2015). Furthermore, for MWCNT-NH₂, at pH=5, which is
276 close to the pKa of NPX, it is observed the highest peak intensity ($E_p = 0.27$ V), thus the
277 reaction is developed at a largest extent. Concerning the peak at $E_p \approx 0.9$ V, it is remarkable
278 the highest peak current in the case of the MWCNT-COOH electrode, that could be consistent

279 with the formation of an uncharged specie, so its interaction with the negative charged surface
280 of this material could favour the reaction.

281 Regarding to the other physical-chemical properties of MWCNTs (S_{BET} , V_{meso} , pore width,
282 electrode surface), no relationship was obtained between them and the MWCNTs behaviour,
283 so only isoelectric point influences the results obtained.

284 The facts previously exposed are congruent with the naproxen oxidation mechanism proposed
285 by Kanakaraju *et al.* (2015) and Montes *et al.* (2016), in which, at deprotonated form the
286 naproxen is oxidized and, after that, a decarboxylation reaction takes place. The uncharged
287 radical formed –hence, lower influence of the pH in this case- is oxidized involving the
288 formation of a cation that is further stabilized.

289 **Reaction mechanism**

290 The liquid medium was analysed by LC-MS after each experiments at different reaction times,
291 in order to identify the reaction products. From the TOC analysis previously shown, it was
292 observed that the NPX of the solution was mineralized in an important extent, so identification
293 of reaction products, previous to total degradation could give information about the reactions
294 pathway. Four reaction intermediates were detected by means of exact mass measurements
295 (m/z of 148, 166, 186 and 202). The $m/z=202$ was detected in all samples, whereas the other
296 compounds were just detected during the first 10 h of reaction in the case of the degradation
297 experiment under fix potential. This fact suggests their complete degradation after this time,
298 which is consistent to the TOC results obtained, or that they are present at very low
299 concentration.

300 With these premises, Figure 7 presents the proposed pathway for the NPX degradation by
301 electroxidation. As it was previously mentioned, the reaction would initiate with the oxidation
302 of the deprotonated form of naproxen molecule following the detailed mechanism of
303 Kanakaraju *et al.* (2015) and Montes *et al.* (2016), yielding 2-acetyl-6-methoxynaphtalene
304 (compound 1), with $m/z = 200$, as well as 2-(1-hydroxyethyl)-6-methoxynaphtalene

305 (compound 2), with $m/z=202$, compound detected in all analysed samples. Likewise, it was
306 described the formation of strong oxidants such as active chlorine species and hydroxyl
307 radicals ($\cdot\text{OH}$). Active chlorine species, mainly chlorine and hypochlorite, can be generated
308 from direct oxidation of the chlorine ion, present in the solution from the NaCl and KCl present
309 in the phosphate buffer (Candia-Onfray *et al.* 2018). The electrolysis of aqueous solution in
310 presence of chlorides could oxidize the reactant to different oxo-chlorinated compounds, but
311 any of these compounds were here detected. Likewise, by anodic discharge of water, $\cdot\text{OH}$
312 radicals which could react either with the reactant or with the intermediates molecules can
313 follow the oxidation reactions (Hamza *et al.*, 2011). In this way, the ionized molecule formed
314 after the second one-electron transfer, could be readily attacked by the electrophilic $\cdot\text{OH}$ and
315 rapidly oxidized (Kuo-Lin Huang 2017). The radical oxidation from the intermediate products is
316 corroborated by the fact that NPX degradation is higher than TOC removal at both stirring
317 speeds and, add to this, the mass transfer limitation influences mainly this electrochemical
318 oxidation, since the NPX removal difference between both speeds (82.5 – 77 %) double the
319 TOC degradation interval (70 – 67 %). This oxidation would yield 1-(6-hydroxynaphthalen-2-
320 yl)ethanone, $m/z = 186$ (compound 3), which can be hydroxylated to compound 4, $m/z=203$.
321 Further degradation of the above mentioned compounds would open an aromatic ring, giving
322 the phthalic acid, $m/z=166$ (compound 5) and m-vinylbenzoic acid $m/z= 148$ (compound 6),
323 which are finally oxidized to CO_2 and H_2O . This oxidation steps from compound 3 to
324 compounds 5 and 6 were already proposed by Coria *et al.* (2016) in the degradation of NPX by
325 Fenton advanced oxidation and by Wang *et al.* (2018) in the degradation by photocatalysis;
326 whereas the final oxidation steps from the open benzoic rings were observed in the
327 paracetamol electrooxidation by Periyasamy and Muthuchamy (2018). The formation of the
328 acidic species in the ring openings justify the decrease in the medium pH with the advanced of
329 the reaction observed by Chin *et al.* (2014) under uncontrolled pH conditions. Likewise, it is
330 remarkable that hydroxyl radicals could be also formed by oxidation of the oxygen molecule,

331 and further decomposition of the hydrogen peroxide formed, being probably this reaction

332 inhibit in acid medium (Periyasamy and Muthuchamy 2018).

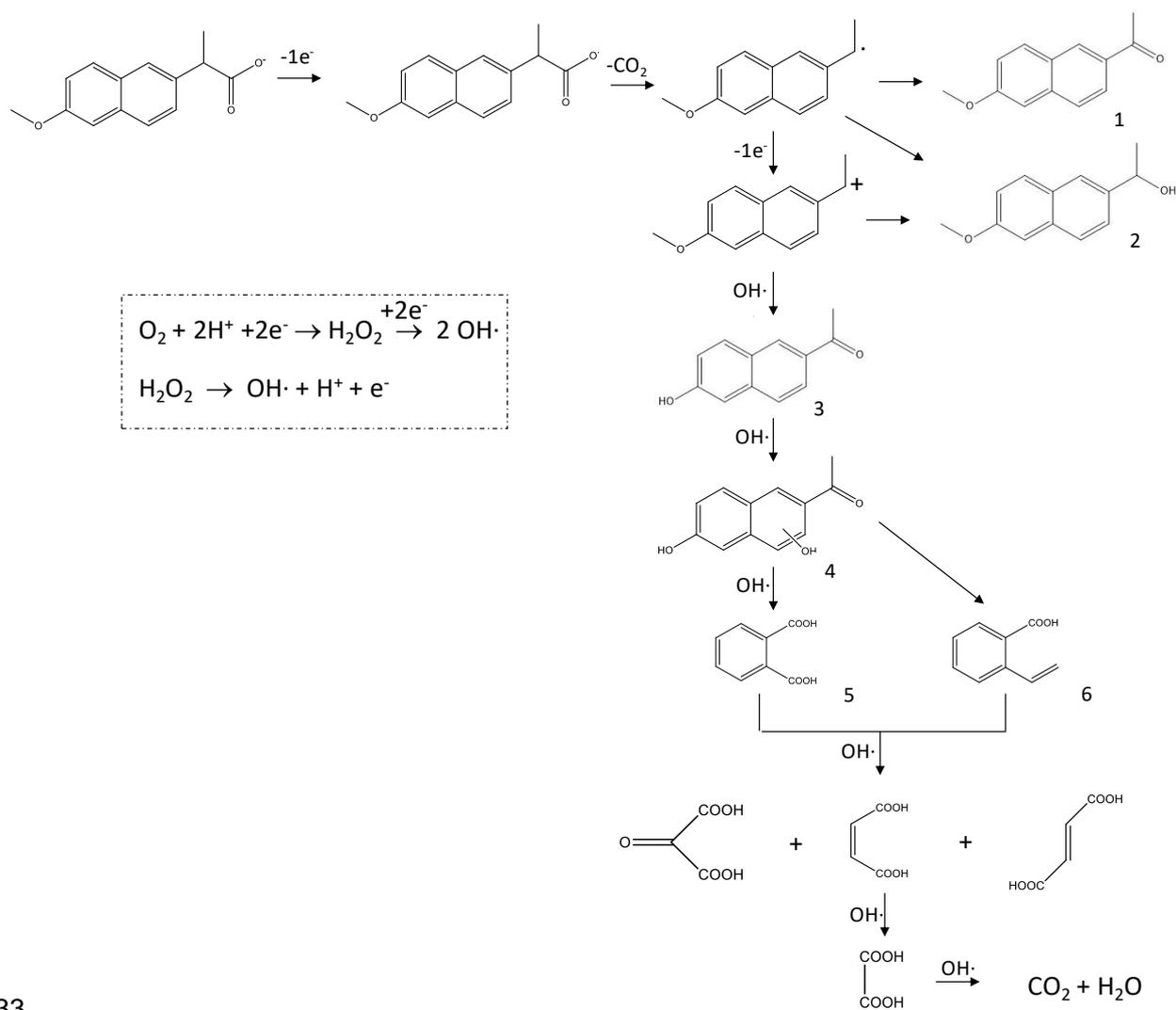


Figure 7. Proposed electrochemical degradation pathway of NPX.

340 Naproxen degradation by cyclic voltammetry, and three different MWCNT working electrodes
341 (MWCNT, MWCNT-COOH and MWCNT-NH₂), was studied. Electrochemical oxidation leads to
342 two oxidation peaks compatible with the oxidation of deprotonated NPX, followed by
343 decarboxylation and further electron transfer oxidation. The mass transfer limits the process
344 as it was deduced from experiences at different scan rates, as well as by the NPX degradation
345 under 500 and 250 rpm stirring speed. In this way, the maximum removal efficiency (82.5%)
346 was reached at constant potential (+1.5V) after 20 hours at 500 rpm. TOC analysis confirm the
347 Naproxen degradation since $TOC/TOC_0 < 30\%$ was obtained.
348 From experiments in the pH range 5-11 it was observed that degradation is favoured at low pH
349 due to the interaction between deprotonated form of the reactant and the surface. Therefore,
350 MWCNT-NH₂, with the highest isoelectric point (4.70) is the most promising material. Further
351 oxidation, carried out on the ionized molecule seems to be more favourable on the MWCNT-
352 COOH material. Subsequent oxidation steps, until mineralization of the NPX, and based on
353 degradation byproducts analysed by LC-MS, are attributed mainly to ·OH.

354

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