

Kinetics of crystal nucleation in ionic solutions: Electrostatics and hydration forces

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Abstract

The heat of precipitation, the mean crystal size and the broadness of crystal size distribution of barium sulfate precipitating in aqueous solutions of different background electrolytes (KCl, NaCl, LiCl, NaBr or NaF), was shown to vary at constant thermodynamic driving force (supersaturation) and constant ionic strength depending on the salt present in solution. The relative inversion in the effect of respective background ions on the characteristics of barite precipitate was observed between two studied supersaturation (Ω) and ionic strength (IS) conditions. The crystal size variance (β^2) increased in the presence of background electrolytes in the order $\text{LiCl} < \text{NaCl} < \text{KCl}$ at $\Omega = 10^{3.33}$ and $\text{IS} = 0.03$ M and $\text{KCl} < \text{NaCl} < \text{LiCl}$ at $\Omega = 10^{3.77}$ and $\text{IS} = 0.09$ M. At a given Ω and IS the respective size of barite crystals decreased with increasing β^2 in chloride salts of different cations and remained constant in sodium salts of different anions.

We suggest that ionic salts affect the kinetics of barite nucleation and growth due to their influence on water of solvation and bulk solvent structure. This idea is consistent with the hypothesis that the kinetic barrier for barium sulfate nucleation depends on the frequency of water exchange around respective building units that can be modified by additives present in solution. In electrolyte solution the relative switchover between long range electrostatic interactions and short range hydration forces, which influence the dynamics of solvent exchange between an ion solvation shell and bulk fluid, results in the observed inversion in the effect of differently hydrated salts on nucleation rates and the resulting precipitate characteristics.

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1. INTRODUCTION

The specific chemistry of a solvent can affect crystal growth and nucleation kinetics, morphology, crystal size distribution and purity of precipitates. In an aqueous solvent, step spreading velocity and rates of surface nucleation have been recognized to depend on ion and surface hydration characteristics. Kinetics of attachment of molecules to a growing phase during crystallization and other phase transition processes have been shown to be limited by the activation energy for diffusion that can result from the need to expel waters attached to the incoming molecules and to the growth site (Petsev et al., 2003). The kinetics of new kink for-

mation (surface nucleation) was hypothesized to depend on the frequency of water exchange between a building unit and a bulk fluid (Kowacz and Putnis, 2008). It has been shown that changing the properties of the aqueous solvation environment by organic additives as well as simple inorganic salts can result in modification of the reaction rates as well as modes of crystal dissolution and growth, surface features, bulk crystal morphology and impurity incorporation even if the thermodynamic driving force is kept constant (De Yoreo and Dove, 2004; Dove et al., 2005; Piana et al., 2006, 2007; Kowacz et al., 2007). The influence of the ionic strength on precipitation kinetics was found to be in agreement with the Bronsted–Bjerrum theory that relates reaction rates with polar properties of the solvent (salt medium effect) and the consequential hydration of ions (Zuddas and Mucci, 1998). The origin of salt-specific effects at constant ionic strength was explained by the fact that the phenomenon of ionic

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strength itself is determined by the water affinity of particular ions (Collins et al., 2007). Consistent with this idea is that the effect of additives on surface processes was recently suggested to result from their influence on solvent structure and dynamics in solvation shells and in the bulk, and not necessarily from specific interactions between species present in solution and the crystal face (Elhadj et al., 2006; Kowacz and Putnis, 2008; Stephenson et al., 2008). Such a concept creates some common framework relating fluid properties and mineral precipitation/dissolution behavior. Recognition of the relation between solution composition, aqueous solvent properties and mineral crystallization can add to our understanding of phase transition processes in multicomponent natural solutions such as seawater or body fluids. It is also of importance for medical and industrial purposes such as inhibition of pathological mineralization, preventing scale formation or designing a product with desirable characteristics such as defined size, morphology and narrow size distribution. Crystal size and crystal size distribution affect dissolution rates and eventual bioavailability, and thus, for example, determine formulation strategies of pharmaceutical products.

This study is concerned with three-dimensional nucleation in multicomponent electrolyte solutions. For the nucleation event to take place in solution, the dissolved ions have to come into contact to form pairs, clusters or aggregates. Association of ions is promoted by the tendency of an aqueous solvent to preserve its hydrogen-bonded network (Hawlicka and Swiatla-Wojcik, 2003). The more structured the solvent the higher its tendency to exclude ions in order to preserve the integrity of the network. Structure (and mobility) of the aqueous solvent depends on solution composition (hydration of solutes and/or the effect of cosolvents) (Hawlicka and Swiatla-Wojcik, 2003; Marcus, 2009). In order to associate, ions have to lose some of their hydration water. Therefore the facility to exchange the water molecules between a solvation shell and the bulk solution also assists association. Dynamics of the solvation shells is affected by the electric fields and hydration properties of the other solutes present in solution (Rull and Ohtaki, 1997; Palka and Hawlicka, 2005). Ion association in solution, the prerequisite for nucleation, depends then on the dynamic and structural characteristics of solvent–solvent and ion–solvent interactions, these being defined by solution composition.

The aim of this work is to investigate the effect of simple ionic salts on three-dimensional nucleation in solution from the perspective of the influence of the electrolytes on solvent structure and on flexibility of ion hydration shells. We present experimental results of barium sulfate precipitation in aqueous solutions of different background electrolytes and address kinetics of nucleation and the resulting characteristics of the precipitate. Electrolyte solution concentrations were adjusted to obtain conditions for which the action of background ions is determined either mainly by their electrostatic influence on ion–water interactions (low ionic strength) or by the effect of their hydration on solvent–solvent interactions (high ionic strength). The composition of background salts was selected to produce distinct electrostatic and hydration characteristics. A calorimetric study on the enthalpy of solution of barium chloride in selected

background electrolytes provided information on the energetical effects of modifying the composition of the aqueous solvent on the solvation of Ba^{2+} ions.

2. METHODS AND MATERIALS

2.1. Experimental procedure

Precipitation experiments were performed in a solution calorimeter (PARR 6755) equipped with a PARR 6772 high-precision thermometer. The experiments were carried out at constant room temperature (25 ± 1 °C) using deionized (MilliQ) water. Each experiment was repeated at least six times. The Dewar flask was filled with 100 ml of 0.033 M or 0.1 M electrolyte solution (KCl, NaCl, LiCl, NaBr or NaF) containing Na_2SO_4 . Ten milliliter of solution containing BaCl_2 in deionized water was loaded into a glass cell sealed with a detachable Teflon dish. The cell was immersed into the Dewar and rotated by an external electric motor. As soon as thermal equilibrium was achieved, the glass cell was opened and the reactants were mixed. The measured temperature change (ΔT_c) due to the exothermic crystallization was used to calculate the heat of barium sulfate precipitation (Q_{BaSO_4}) in respective background salts. ΔT_c was converted to heat (Q_{BaSO_4}) by multiplying ΔT_c by the energy equivalent (e) of the calorimeter and its contents: $Q_{\text{BaSO}_4} = \Delta T_c \cdot e$ (e was derived by a pre-experimental standardization process). Immediately after the crystallization reaction had taken place (as indicated by abrupt temperature change followed by lag period) 15 ml of the resulting solution was filtered through a filter with 0.45 μm pore diameter. The filtrate was then analyzed with ICP-AES (inductively coupled plasma atomic emission spectroscopy) using an iCAP 6000 (Thermo) plasma spectrometer for $[\text{Ba}^{2+}]$ concentration. The precipitate remaining on the filter was imaged by scanning electron microscopy (SEM) and analyzed by X-ray diffraction. Heat of dilution of the BaCl_2 solution (from 10 to 110 ml) in the solution of background electrolyte was equal within an experimental error for all of the background salts and therefore the heat of dilution was not included in the calculation of Q_{BaSO_4} . The calorimetric data reported in this work are then used to compare the relative effects of different background electrolytes and not to derive absolute values. The enthalpy of BaSO_4 precipitation (ΔH_{ppt}) was calculated as: $\Delta H_{\text{ppt}} = (-Q_{\text{BaSO}_4})/N$, where N is the number of moles of BaSO_4 determined by comparing the final concentrations of barium in the aqueous solution to their initial values (under assumption that all the $[\text{Ba}^{2+}]$ consumed during the crystallization process is taken up by the stoichiometric precipitation of BaSO_4).

The solution composition, the supersaturation (Ω) with respect to barium sulfate, the experimentally determined Q_{BaSO_4} , ΔH_{ppt} and the measured concentration of $[\text{Ba}^{2+}]$ left in solution after the crystallization process are presented in Table 1. The error in the final barium concentrations represents the reproducibility involved in the whole precipitation procedure. The saturation state is expressed as $\Omega = \text{IAP}/K_{\text{sp}}$ (IAP—ion activity product; K_{sp} —solubility product). The computer program PHREEQC (Parkhurst and Appelo, 1999) was used to calculate the saturation index $\text{SI} = \log(\text{IAP}/K_{\text{sp}})$ and ionic

Table 1

Solution composition (after mixing in the final 110 ml) used in the experiments (initial concentration) and associated data: Ω —supersaturation with respect to BaSO_4 ; concentration of $[\text{Ba}^{2+}]$ measured in solution after precipitation reaction (final concentration) expressed in μM and as the percentage of barium remaining in solution with respect to the initial value (relative $[\text{Ba}^{2+}] = \% \text{ of init. } [\text{Ba}^{2+}]$); Q_{BaSO_4} —heat of BaSO_4 precipitation; ΔH_{ppt} —enthalpy of precipitation; average crystal size (X-rays)—average crystal size determined by X-ray diffraction method; mean crystal size (\bar{X})—mean crystal size calculated by CrystalCounter program based on measurements done with Image Tool; β^2 —the variance of the natural logarithms of the sizes; CSD shape—shape of crystal size distribution.

Background electrolyte	Initial concentration		Ω	Final concentration		Q_{BaSO_4}		ΔH_{ppt} (kJ/mol)	Average crystal size (X-rays) (μm)	Mean crystal size (\bar{X}) (μm)	β^2	CSD shape		
	Electrolyte (M)	$[\text{Ba}^{2+}] = (\mu\text{M})$		$[\text{SO}_4^{2-}] = (\mu\text{M})$	$[\text{Ba}^{2+}] = (\mu\text{M})$	$[\text{Ba}^{2+}] = \% \text{ of init. } [\text{Ba}^{2+}]$	(J)						STDEV \pm (J)	
LiCl	0.09	2640	2640	$10^{3.78}$	63.26	9.75	2.46	9.84	0.55	-3.82	11.54	7.82	0.285	Lognormal
NaCl	0.09	2640	2640	$10^{3.77}$	95.06	5.72	3.74	7.01	0.76	-2.75	13.27	8.20	0.280	Lognormal
KCl	0.09	2706	2706	$10^{3.77}$	134.22	14.99	5.22	8.77	0.15	-3.41	28.48	13.53	0.132	Lognormal
NaCl	0.03	1320	1320	$10^{3.47}$								6.44	0.159	Lognormal
LiCl	0.03	330	5280	$10^{3.33}$	0.25	0.12	0.08	2.26	0.30	-6.84		9.21	0.068	Lognormal
NaCl	0.03	330	5280	$10^{3.33}$	0.06	0.03	0.02	3.47	1.07	-10.51	5.89	6.40	0.088	Lognormal
KCl	0.03	330	5280	$10^{3.33}$	0.39	0.12	0.12	2.56	0.11	-7.77		5.07	0.125	Lognormal
NaF	0.03	330	5280	$10^{3.33}$	0.32	0.24	0.10	2.77	0.42	-8.41	5.80	5.98	0.134	Lognormal
NaBr	0.03	330	5280	$10^{3.33}$	0.27	0.11	0.08	2.42	0.87	-7.33		6.00	0.055	Lognormal

Table 2

Enthalpy of solution of $\text{BaCl}_2 \times 2\text{H}_2\text{O}$ (ΔH_{BaCl_2}) in electrolyte solutions.

Electrolyte		ΔH_{BaCl_2}
Type	Conc. = (M)	(kJ/mol)
LiCl	0.1	15.53
NaCl		13.57
KCl		14.08
LiCl	0.03	13.33
NaCl		12.61
KCl		14.44

strength (IS). The concentration of $[\text{Ba}^{2+}]$ and $[\text{SO}_4^{2-}]$, background salts and Ω express concentrations of species and the saturation state of the system that would be achieved in case of complete mixing of working solutions in the final 110 ml of solution. Nevertheless it is worth noting that supersaturation in fact develops during the time of the mixing process. Moreover $[\text{Ba}^{2+}]$ in solution is initially concentrated in a volume ten times smaller than the $[\text{SO}_4^{2-}]$. As a result the actual Ω in a real reaction time can be different from the calculated “nominal supersaturation”.

The enthalpy of solution of barium chloride dihydrate ($\text{BaCl}_2 \times 2\text{H}_2\text{O}$) in selected background electrolytes was determined by loading a glass cell of the calorimeter with a 0.15 g sample of solid $\text{BaCl}_2 \times 2\text{H}_2\text{O}$ and dissolving the solid in the Dewar flask containing 100 ml of 0.03 M or 0.1 M KCl, NaCl or LiCl aqueous solution. The calculated heat of solution ($Q_{\text{BaCl}_2} = \Delta Tc \cdot e$) was converted to enthalpy of solution (ΔH_{BaCl_2}) according to the formula: $\Delta H_{\text{BaCl}_2} = (-Q_{\text{BaCl}_2})/N$, where Q_{BaCl_2} is expressed in kJ and N in moles of $\text{BaCl}_2 \times 2\text{H}_2\text{O}$. ΔH_{BaCl_2} provides information about the solvation of Ba^{2+} in aqueous solutions of different chloride salts. The results are presented in Table 2.

2.2. Average crystal size

The average size of the crystals obtained in the precipitation experiments was determined from two-dimensional X-ray diffraction patterns collected using a single-crystal diffractometer equipped with an X-ray area detector (CCD). X-ray area detectors were initially used for protein crystallography in the 1980s, but more recently their use has been extended to a number of applications, including the study of polycrystalline materials (He, 2005). Two-dimensional diffraction patterns of polycrystalline samples consist of concentric (Debye–Scherrer) rings associated with different Bragg reflections. Each ring is produced by the superposition of reflections of many crystals illuminated by the X-ray beam, all of them with a set of $(h k l)$ crystallographic planes oriented to fulfil the Bragg condition. These 2D-diffraction patterns can be converted into conventional diffractograms (2θ -scans) by radial integration of pixel intensities. These conventional diffractograms can be processed as usual for mineral phase identification, crystallinity and crystallite size measurements, refinement of cell parameters, etc. However, the 2D-diffraction pattern contains additional information about the grain size, the existence of preferential orientations, and other textural features.

For instance, depending on the specific characteristics of the sample, the rings can be continuous or spotty. When a ring is spotty, the variation of intensity along a ring associated with a given hkl reflection (ψ -scan) gives an intensity profile (after azimuthal integration) with a series of peaks. In a ψ -scan, each peak corresponds to the reflection from an individual crystal with the corresponding (hkl) planes oriented to fulfil the Bragg condition. These ψ -scan peak intensities depend on the crystal size: as the average crystal size increases, the peak intensities increase and the number of peaks decreases. From the average intensity of these peaks and using a calibration curve obtained with standard samples, the crystal size can be determined. It is worth noting that the crystal size determined in this way represents the real average physical size, a parameter that may be com-

pletely different from the so-called crystallite size. The crystallite size is an XRD term that indicates the size of a coherently diffracting domain and thus does not necessarily coincide with the crystal size. This latter parameter is usually determined by considering the full width at half maximum of a given reflection in a conventional 2θ -scan.

Here, the two-dimensional X-ray diffraction patterns of the precipitates have been obtained using an Oxford Diffraction Xcalibur Nova single-crystal diffractometer equipped with a CCD area detector Onyx (165 mm) and Cu-K α radiation. The precipitate samples were glued to a fibre (the type commonly used for mounting single crystals) and placed at a distance to the detector of 65 mm. The 2D-patterns (Fig. 1a) were then studied using the *XRD2DScan* software (Rodríguez-Navarro, 2006). The samples were first

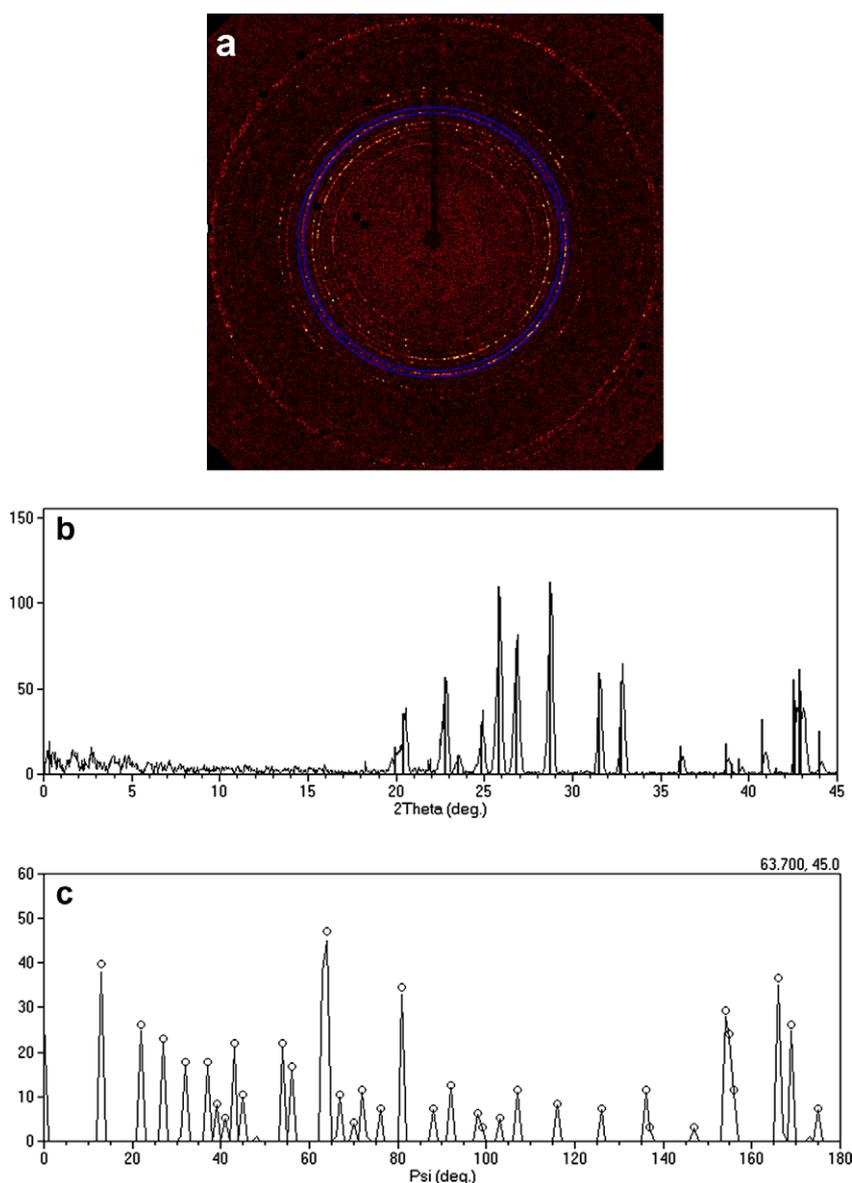


Fig. 1. (a) Two-dimensional diffraction pattern of a sample of the precipitate obtained in experiment 331-Na. The blue line delimits a ring associated with the 1 2 1 reflection of barite. (b) 2θ -Scan and peaks of the 24–1035 card (Barite, Pbnm). (c) ψ -Scan of the ring masked in (a). (For interpretation of color mentioned in this figure the reader is referred to the web version of the article.)

identified to be barite by analyzing the reflections in a conventional 2θ -scan diffractogram (Fig. 1b). Then, in order to perform the crystal size study, the reflection 1 2 1 ($2\theta = 28.744^\circ$) was selected. This is one of the three main reflections of barite and is usually very well defined in the diffractograms. Fig. 1c shows the variation of intensity along the 1 2 1 ring as a function of the ψ -angle (from 0 to 180°) in the case of the sample 331-Na. These ψ -scans were calculated by integrating pixel intensities within a 2θ range from $\sim 28.4^\circ$ to $\sim 29.3^\circ$. The *XRD2DScan* software determines the number of peaks and the average peak intensity. From this average value, and using a calibration curve, the average crystal size can be determined. Here, this calibration curve was obtained using barite grains of known size. Table 1 shows the crystal sizes determined in this way.

2.3. Crystal size distribution (CSD)

SEM images of the barium sulfate precipitate were processed with the UTHSCSA Image Tool computer software (developed at the University of Texas Health Science Center at San Antonio, Texas and available from the Internet by anonymous FTP from maxrad6.uthscsa.edu) to determine the sizes of the individual barite crystals representative for the size distribution of the crystals that precipitated in different electrolytes. In all experiments the resulting precipitate has a plate-like morphology (Fig. 2) and therefore the area of the best expressed crystal face was used in this work as an indication of the relative size of the crystal. Crystal size was then described by the diameter of the square with the same area as the measured area of the respective crystal face. The crystal diameters estimated in this way (approximately 100 for each sample) were used to generate crystal size distributions with the program CrystalCounter (Eberl et al., 2000). The program calculates CSD shape, the mean crystal size ($\bar{X} = \sum Xf(X)$, where $f(X)$ is the frequency of group size X), the mean of the natural logarithms of the sizes ($\alpha = \sum \ln(X)f(X)$), and the variance of the natural

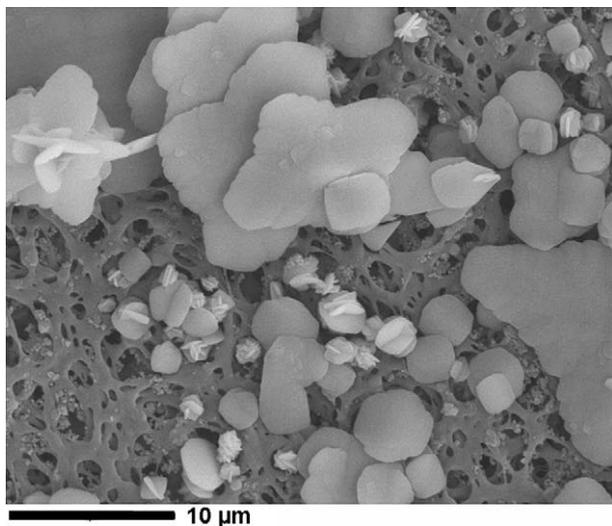


Fig. 2. SEM image showing barite crystals precipitated in the presence of 0.09 M NaCl as background electrolyte.

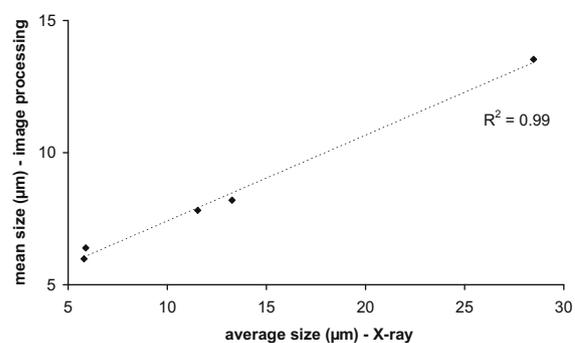


Fig. 3. Correlation between mean crystal size (\bar{X}) and average crystal size of barium sulfate precipitate derived by image processing and X-ray diffraction method, respectively.

logarithms of the sizes ($\beta^2 = \sum (\ln X - \alpha)^2 f(X)$). According to the approach proposed by Eberl et al. (1998), CSD shapes can be related to the crystal growth mechanism. Three basic CSD shapes corresponding to different growth modes are: (a) an asymptotic CSD produced in systems with constant-rate nucleation followed by size-dependent (proportional) surface controlled growth; (b) universal, steady-state curve attributed to Ostwald ripening, and (c) lognormal (one of the most common CSD in natural systems (Eberl et al., 2002)) generated by a crystal growth mechanism having decaying-rate nucleation accompanied by size-dependent growth. Size-dependent growth means that crystal growth rate is proportional to the initial crystal size, so that larger crystals grow faster than smaller crystals leading to increasing crystal size variance (β^2) with time. Calculated mean crystal sizes (\bar{X}), crystal size variance (β^2) and CSD shapes are reported in Table 1.

Because of the complex morphology of the crystals, sizes determined by image processing (IP) are not a very accurate expression of the actual dimensions of the crystalline material. Therefore for selected samples, calculated mean crystal sizes determined from SEM images were compared with average crystal sizes determined by the X-ray diffraction method. The X-ray method probably gives a better estimation of the actual mean crystal size, but it has the disadvantage that does not allow estimating the CSD. Thus, as we need to determine the CSD we have used the IP method and the X-ray method is used just to check if there is a good correlation with the mean sizes obtained by the IP. The trends in the relative differences in sizes of the crystals that precipitated in respective background electrolytes at given experimental conditions are in good agreement between the two methods (Fig. 3). The actual values are different, but sizes obtained by X-ray diffraction correlate with real crystal volume, while those based on image processing correlate with the area of the imaged faces only.

3. RESULTS

In all our experiments barium sulfate crystals are log-normally distributed (Table 1 and Fig. 4) implying a common nucleation and growth mechanism (Eberl et al., 1998). At the same time crystal size (\bar{X}) and broadness of crystal size distribution (β^2) vary at constant ionic strength

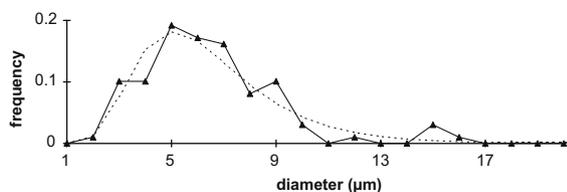


Fig. 4. Example of the crystal size distribution (CSD) of barium sulfate precipitated in 0.03 M NaCl as a background electrolyte. Lognormal distribution was verified by the K–S (Kolmogorov–Smirnov) statistical test that compares CSD generated by Crystal-Counter (Eberl et al., 2000) based on the introduced data (solid line) with theoretical lognormal CSD (dashed line).

(IS) and constant thermodynamic driving force (supersaturation) depending on the background electrolyte present in solution (Table 1). The specific correlations are outlined below and presented explicitly in Fig. 5.

Chloride electrolytes (with different cations: Li^+ , Na^+ and K^+):

- At $\Omega = 10^{3.33}$ and IS = 0.03 M, β^2 increases in the order $\text{LiCl} < \text{NaCl} < \text{KCl}$.
- At $\Omega = 10^{3.77}$ and IS = 0.09 M, β^2 increases in the order $\text{KCl} < \text{NaCl} < \text{LiCl}$, that is, the effect is the reverse.
- With KCl as background electrolyte the mean crystal size (\bar{X}) is considerably larger at $\Omega = 10^{3.77}$ (and IS = 0.09 M) than at $\Omega = 10^{3.33}$ (and IS = 0.03 M).
- With NaCl as background electrolyte the mean crystal size (\bar{X}) is only slightly larger at $\Omega = 10^{3.77}$ (and IS = 0.09 M) than at $\Omega = 10^{3.33}$ (and IS = 0.03 M). (At constant IS = 0.03 M changing Ω does not seem to affect \bar{X}).
- With LiCl as background electrolyte the mean crystal size (\bar{X}) is smaller at $\Omega = 10^{3.77}$ (and IS = 0.09 M) than at $\Omega = 10^{3.33}$ (and IS = 0.03 M) (the effect is the reverse to that of KCl).
- For a given supersaturation ($\Omega = 10^{3.33}$ or $\Omega = 10^{3.77}$) and IS the mean crystal size (\bar{X}) decreases with increasing β^2 .
- For a given background electrolyte, β^2 increases with increasing Ω and IS. The effect is less marked with KCl.

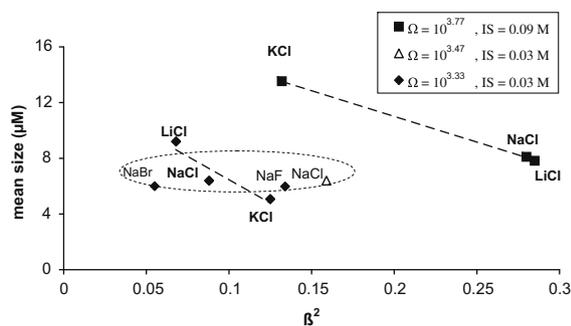


Fig. 5. Mean crystal size (\bar{X}) of barium sulfate precipitate at different supersaturation (Ω) and IS conditions as a function of crystal size variance (β^2). The dashed lines show the tendencies for different chlorides, whereas the short-dash ellipse shows the tendency for different sodium halides.

Sodium electrolytes (with different anions: Br^- , Cl^- and F^-):

- At $\Omega = 10^{3.33}$ and IS = 0.03 M the mean crystal size (\bar{X}) is virtually the same for all the three electrolytes.
- β^2 depends on the background salt type, increasing in the order $\text{NaBr} < \text{NaCl} < \text{NaF}$.

The enthalpy of precipitation of barium sulfate depends on the background electrolyte and is less negative at higher Ω and IS (Table 1). The enthalpy of precipitation is given by: $\Delta H_{\text{ppt}} = U(\text{BaSO}_4) - \Delta H_{\text{hyd}}(\text{Ba}^{2+}) - \Delta H_{\text{hyd}}(\text{SO}_4^{2-})$, where $U(\text{BaSO}_4)$ is the lattice energy, $\Delta H_{\text{hyd}}(\text{Ba}^{2+})$ and $\Delta H_{\text{hyd}}(\text{SO}_4^{2-})$ are the enthalpies of hydration of the ions. Because lattice energy does not depend on solution composition, the less negative ΔH_{ppt} implies higher energy expended on dehydration of the ions (enhanced ion–water attraction) at higher IS.

Enthalpy of solution of $\text{BaCl}_2 \times 2\text{H}_2\text{O}$ (ΔH_{BaCl_2}) depends on the ionic strength and on the salt type (Table 2). ΔH_{BaCl_2} results from the energy expended on breaking solute–solute bonds (here constant lattice energy) and solvent–solvent interactions and the energy gain on ion solvation. Therefore, as the energy involved in solute–solute bonds does not depend on the background electrolyte, ΔH_{BaCl_2} in different chloride salts is expected to be an indication of the relative changes of water–water vs. barium–water interactions in respective electrolytes. Consequently less positive ΔH_{BaCl_2} at higher KCl concentration implies more energetically favorable hydration of Ba^{2+} while more positive ΔH_{BaCl_2} at higher NaCl and LiCl concentration indicates less favorable hydration of Ba^{2+} at higher IS. The hydration in this context is defined by the relative difference in the affinity of water to the ion and the affinity of water to other water molecules (Samoilov, 1965).

4. DISCUSSION

The observed dependence of the characteristics of the solid (β^2 and \bar{X}) precipitated at constant Ω (by a common mechanism as indicated by CSD shape) on the solution composition (Fig. 5) can be explained by considering differences in the reaction kinetics. A lognormal distribution of barium sulfate crystals precipitated in our experiments indicates that crystals were generated in systems with a decaying nucleation rate accompanied by size-dependent crystal growth (Kile et al., 2000). Such a crystal size distribution suggests that nucleation and growth is controlled by advection rather than diffusion of the reactants (Kile and Eberl, 2003). In our experimental procedure supersaturation (Ω) buildup starts after mixing the working solutions. The theoretical supersaturation level that could be achieved in the system is very high. However, because of a very short induction period the actual Ω cannot exceed the threshold value over which the nucleation rate surpasses the mixing velocity, so that Ω is limited by crystal precipitation (Söhnel and Mullin, 1987; Philips et al., 1999; Kile et al., 2000; Vicum et al., 2003; Schwarzer and Peukert, 2004). As a result the first nucleating particles grow while further nuclei are simultaneously generated. The longer the period of nucle-

ation the higher the resulting crystal size variance (β^2) (Phillips et al., 1999). For a given nominal supersaturation and mixing velocity (as applied in this work), the period in which nucleation and growth coexist depends on the induction time (τ) for nucleation, because the shorter the induction time the higher the number of nucleation events during the “mixing period”. As a consequence, β^2 is proportional to τ^{-1} . Moreover, as τ is inversely proportional to the nucleation rate, β^2 results to be an indication of the nucleation kinetics. The variance of the CSD yields information about nucleation and initial growth conditions because, during the first few nanometers of growth (as relevant for our experiments), the β^2 changes in response to solution chemistry (Eberl et al., 1998).

The observation that means crystal size decreases with increasing β^2 (for different chloride salts at constant Ω) is consistent with conclusion that in the investigated system β^2 tracks nucleation rates. In our experiments the only variable (for a given Ω and IS) is the background electrolyte. Therefore differences in the kinetics of barium sulfate crystallization and consequent crystal size variance and mean crystal size result from the influence of background ions.

4.1. Frequency of water exchange as rate-limiting factor for nucleation

According to the classical nucleation theory increasing the supersaturation and/or reducing the solid–liquid interfacial tension lowers the nucleation barrier. The height of the nucleation barrier, in the case of spherical nuclei, is expressed by free energy of formation of critical nuclei:

$$\Delta G^* = \frac{16\pi}{3} \gamma^3 / \rho |\Delta\mu|^2, \quad (1)$$

where γ is the solid–liquid interfacial tension, ρ is the number density of a crystal phase, $\Delta\mu = \mu(\text{BaSO}_4)_{(s)} - \mu(\text{Ba}^{2+})_{(aq)} - \mu(\text{SO}_4^{2-})_{(aq)}$ (where μ designates the chemical potential of respective species in the solid (s) and the liquid state (aq)). The rate J at which nuclei are formed depends exponentially on ΔG^* :

$$J = \kappa \exp(-\Delta G^*/k_B T) \quad (2)$$

where k_B is Boltzmann’s constant and κ is a kinetic prefactor.

Our experimental observations suggest that nucleation rates of barite (as predicted by β^2) vary in different background electrolytes regardless of the same Ω (i.e. constant $\Delta\mu$) (Table 1 and Fig. 5). Therefore, from Eq. (2), differences in the nucleation rates of barite are determined by differences in the kinetic barrier for nucleation (κ) and/or surface tension (γ). The kinetic prefactor (κ) is proportional to the diffusion coefficient of crystal building units (Walton, 1969; Jones et al., 2005). Diffusion of ions in aqueous solutions is determined by the frequency of water exchange ($f_{\text{H}_2\text{O}}$) between an ion solvation shell and a bulk fluid (Lee and Rasaiah, 1994, 1996; Chong and Hirata, 1999; Rasaiah and Lynden-Bell, 2001; Du et al., 2007), which depends on the competition between the tendency of the ion to orient water molecules in its solvation shell and the tendency of the water to preserve its hydrogen-bonded net-

work (Hribar et al., 2002). Solid–liquid interfacial tension is also defined by the competition between cohesive forces of the liquid and adhesive forces between water molecules and the solid surface. Therefore $f_{\text{H}_2\text{O}}$ (hence κ) and γ are in fact correlated. A longer residence time of water in the vicinity of an ion (as a result of enhanced ion–water or reduced water–water affinity) means a less favorable κ but lower interfacial tension. This implies that the same changes in solution can cause opposite effects on nucleation rate. This is in agreement with AFM (Kowacz et al., 2007) and molecular simulation studies (Piana et al., 2006; Jones et al., 2008) that have shown that addition of methanol to an aqueous solution increases kinetics of two-dimensional (2D) nucleation on a barite surface in spite of the increase in γ . These findings were attributed to the reduced kinetic barrier of cation desolvation as a result of the strengthening of H-bonds in the aqueous solvent. The frequency of water exchange around crystal building units was then suggested to be the rate-limiting factor for surface-controlled 2D nucleation of barium sulfate (Kowacz and Putnis, 2008) because it defines the probability of contact of the ion in its “dehydrated state” with the crystal surface. Such an effective contact, the starting point for a nucleation event, can mean that an ion is moved to a position where it shares its water of solvation with the surface (or with another ion in solution) so that its position at the surface (or in the vicinity of the ion) is stabilized with respect to its residence in the bulk. The results presented here suggest that ion dehydration rates also control three-dimensional nucleation of barite in solution.

4.2. Long range electrostatic interactions and short range hydration forces as controls of water exchange frequency

The dependence of the nucleation rates of barite (as indicated by β^2) on the background salt (at given Ω and IS) and the relative switchover in the effect of respective electrolytes on nucleation kinetics between the two studied Ω (and IS) conditions (Fig. 5) can be explained by considering factors affecting dehydration rates of ions immersed in electrolyte solution. The dehydration and association of ions will be affected by the facility to strip water molecules from the ion solvation shell and by the tendency of the structured fluid to exclude ions from its H-bonded network.

The frequency of water exchange ($f_{\text{H}_2\text{O}}$) around an ion is defined by the ratio (τ_i/τ_0) of the residence time of a water molecule in the closest position to the ion (τ_i), to the residence time of water in the bulk (τ_0). In electrolyte solution the potential energy of a water molecule oriented in an ion solvation shell (here we consider Ba^{2+} and SO_4^{2-}) is lowered by attractive interaction between the partial charge of the water dipole and the unlike electric field of counterions (components of background salt) (Samoilov, 1967, 1971). As a result the position of a water of solvation of an ion immersed in electrolyte solution is stabilized and the residence time of this water ($\tau_{i\text{-salt}}$) increases in salt solution in comparison to pure water (τ_i) (Kinoshita and Harano, 2005).

The mean time during which two solvent molecules stay in the immediate vicinity of each other in the electrolyte solution ($\tau_{0\text{-salt}}$) depends on the effect of the electrolyte on

water structure dynamics. The higher the potential of background ions to orient water in their solvation shells (hydration) the more retarded is the mobility of water molecules in solution ($\tau_{0\text{-salt}}$ increases). When high charge density of the ion retards water mobility in its vicinity compared to mobility within the hydrogen-bonded network of bulk water ($\tau_i > \tau_0$) the hydration of an ion is defined as “positive”. Examples are Na^+ , Li^+ and F^- . When the water mobility is increased in its vicinity compared to in the bulk ($\tau_i < \tau_0$) the hydration of an ion is “negative”, e.g. K^+ , Cl^- , Br^- (Samoilov, 1965).

At $\text{IS} = 0.03 \text{ M}$ (lower electrolyte concentration) the $f_{\text{H}_2\text{O}}$ around Ba^{2+} and SO_4^{2-} (hence diffusion of the ions) is controlled by the “electrostatic environment”, which is related to the nature of the background electrolyte, particularly to the tendency to form ion pairs ($\text{KCl}_{(\text{aq})}$, $\text{NaCl}_{(\text{aq})}$, etc.). For simple 1:1 electrolytes this tendency is related to the electrolyte solubility: the lower the solubility the higher the tendency of the electrolyte cations and anions to pair (Collins, 1995, 1997), which decreases the effect of their charges on the residence time of water of hydration ($\tau_{i\text{-salt}}$) and thus on the mobility of Ba^{2+} and SO_4^{2-} . Therefore the mobility of Ba^{2+} and SO_4^{2-} is higher in less soluble salts and the nucleation rate of barite increases with decreasing solubility of background electrolyte (Fig. 6).

Ion distribution in solution (and solubility of simple ionic salts) depends on hydration characteristics. Similarly hydrated ions tend to associate while oppositely-hydrated ions tend to stay apart in solution (Hawlicka and Swiatla-Wojcik, 2003; Collins et al., 2007). As a result the kinetics of barite nucleation is faster in background salts composed by ions of the same (positive–positive or negative–negative) hydration compared to salts composed of ions of opposite (positive–negative) hydration. This can be illustrated by the noticeably higher β^2 in KCl with respect to NaCl as background electrolyte regardless of a very small difference in the solubility of these salts (Fig. 6).

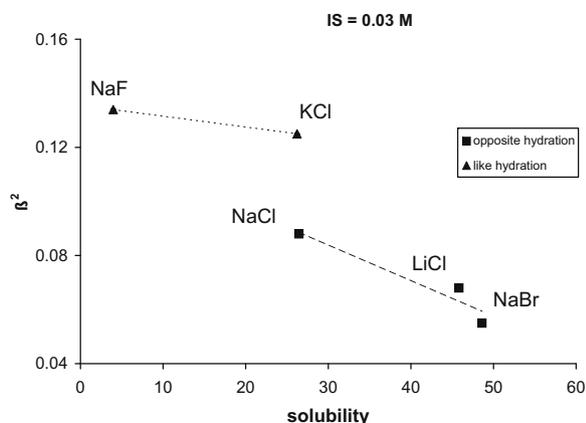


Fig. 6. Crystal size variance (β^2) of barium sulfate precipitate as a function of solubility of background salt at ionic strength ($\text{IS} = 0.03 \text{ M}$) and supersaturation ($\Omega = 10^{3.33}$). Trend lines follow β^2 in salts composed of ions of the same (“like-hydration”— NaF , KCl) and unlike (“opposite-hydration”— NaBr , LiCl , NaCl) hydration characteristics. Solubility is expressed as a mass percent of solute (Lide, 2004).

At $\text{IS} = 0.09 \text{ M}$ (higher electrolyte concentration), where electrostatic interactions are suppressed and hydration shells overlap, the differences in the $f_{\text{H}_2\text{O}}$ around Ba^{2+} and SO_4^{2-} in respective background electrolytes are no longer controlled by the “electrostatic environment” (ion charge distribution) but by the effect of the electrolyte ions on the bulk solvent structure dynamics ($\tau_{0\text{-salt}}$). The higher the affinity of water to other solvent molecules (other waters or ions) in electrolyte solution, the less mobile and less prone the water will be to hydrate solutes (Ba^{2+} and SO_4^{2-}) immersed in the electrolyte solution. Therefore, nucleation rates of barite increase with increasing positive hydration of background cation (the anion is common for all background electrolytes) (Fig. 7). This can be understood from the perspective of the competition for hydration water between background ions and barite building units: the higher the competition the faster the frequency of water exchange. Such a conclusion is consistent with Raman spectral studies showing the effect of hydration of counterion (Rb^+ , Cs^+ , K^+ , Na^+ , Li^+) on frequency of water exchange around SO_4^{2-} (Rull and Ohtaki, 1997). The difference in the effect of background ions on the nucleation rate of barite is the most strongly expressed between solutions of chloride salt of negatively hydrated K^+ and solutions of chloride salts of positively hydrated Na^+ and Li^+ . The effect of positively hydrated ions is very similar in spite of the significant difference in their hydration energy. Nevertheless the mobility of water in electrolyte solutions (therefore the residence time of water in the vicinity of other water molecules) depends not only on the energy of ion–water

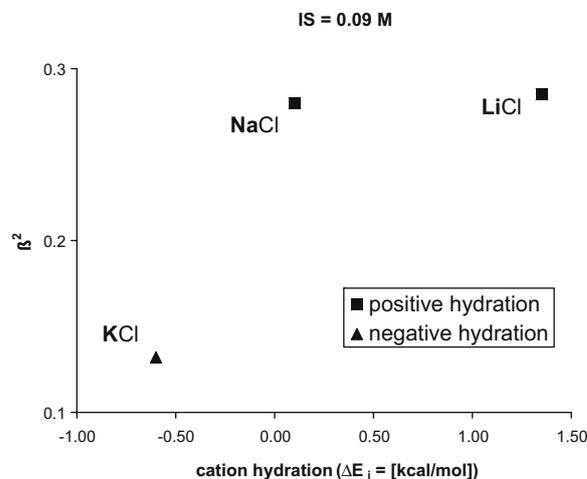


Fig. 7. Crystal size variance (β^2) of barium sulfate precipitate as a function of hydration (ΔE_i) of background cation ($i = \text{K}^+$, Na^+ , Li^+) of respective chloride salt at ionic strength ($\text{IS} = 0.09 \text{ M}$) and supersaturation ($\Omega = 10^{3.77}$). Hydration values are taken from Chong and Hirata (1997) and expressed as a difference (ΔE_i) in the activation energy of removing a water molecule from the ion solvation shell (E_i) and the activation energy of transferring a water molecule from the first to the next coordination shell of another water molecule (E_0), i.e. $\Delta E_i = E_i - E_0$ (Samoilov, 1965). $\Delta E_i < 0$ corresponds to “negative hydration” (enhanced translational motion of water molecules in the vicinity of the ion, $\tau_i < \tau_0$) and $\Delta E_i > 0$ to “positive hydration” (retarded water mobility in the adjacent environment of the ion, $\tau_i > \tau_0$).

interaction, but is defined by the structure of water modified by the ion (Koneshan et al., 1998). Experimental results show that the mobility of water is significantly different in KCl solution in comparison to the relatively small differences in water mobility in NaCl and LiCl (Ionov and Mazitov, 1968).

The inversion in the influence of different chloride salts on the reactivity of barite with increasing ionic strength is consistent with our previous AFM observations (Kowacz and Putnis, 2008). Such an effect can be explained by considering the fact that the frequency of water exchange around solute ions (here Ba^{2+} and SO_4^{2-}) is a result of a competition between the tendency of the solute to orient water in its solvation shell and the tendency of a solvent to preserve its structure, both factors that are affected by different properties of the electrolyte solution. The solute–water affinity is affected by propagation of electric fields of background ions, the property that is most expressed at low ionic strength conditions. The dynamics of the solvent structure is affected by the hydration characteristics of the individual background ions, the property that becomes most pronounced at higher ionic strength. The relative switchover between long range electrostatic interactions and short range hydration forces is in agreement with the fact that in the limit of dilute solutions, thermodynamic properties of electrolytes can be approximated by continuum electrostatics, but when the ionic strength is greater than $\sim 1 \times 10^{-2}$ M, charge propagation (Debye length) is comparable or smaller than the size of water molecules (Akiyama et al., 2007) and the thermodynamic behavior of the electrolyte depends significantly on the effect of ions on solvent structure and dynamics (Conway and Ayranci, 1999; Petsev and Vekilov, 2000; Kunz et al., 2004; Collins et al., 2007).

4.3. Activation energy of nucleation and growth

The information about the nucleation rate and the amount of barite precipitate that has been generated in solutions of different background electrolytes allows us to extract some information about the relative input of the nucleation vs. growth process in solid formation in respective solutions. The calorimetric study then provides information about the energetical response of the system to specific processes in crystal formation. This data is then correlated with the relationship between the fundamental steps in the crystallization process and the respective phenomena involving rearrangement of solvent molecules around solutes and around other solvent molecules in the bulk.

The relative amounts of $[\text{Ba}^{2+}]$ that have been consumed during the crystallization process (assumed to be proportional to the amount of precipitate) correlates with solubility at lower ionic strength and hydration of the background electrolyte at higher ionic strength conditions and therefore with predicted nucleation rates (Figs. 8 and 9).

However the correlation between the solubility of the background salt and the relative amount of barium sulfate precipitate follows different trend lines for the crystallization process in salts composed of oppositely-hydrated (i.e. NaBr, LiCl and NaCl) and like-hydrated (i.e. KCl and

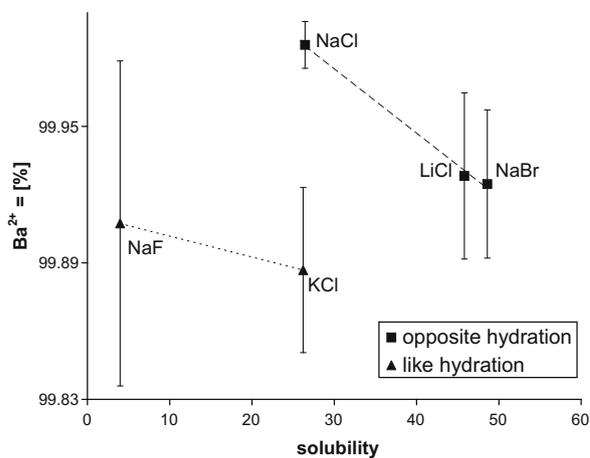


Fig. 8. Relative amounts of Ba^{2+} (as a percent of initial Ba^{2+} concentration in solution) consumed during crystallization process as a function of solubility of background salt at ionic strength (IS) = 0.03 M and supersaturation (Ω) = $10^{3.33}$. Amount of Ba^{2+} represents an average value from the precipitation experiments in the presence of the respective background salt, and the error bars represent one standard deviation about that mean.

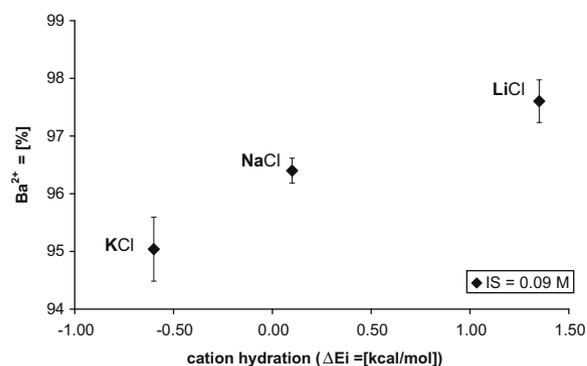


Fig. 9. Relative amounts of Ba^{2+} (as a percent of initial Ba^{2+} concentration in solution) consumed during crystallization process as a function of hydration (ΔE_i) of background cation ($i = \text{K}^+$, Na^+ , Li^+) of respective chloride salt at ionic strength (IS) = 0.09 M and supersaturation (Ω) = $10^{3.77}$. Amount of Ba^{2+} represents an average value from the precipitation experiments in the presence of the respective background salt, and the error bars represent one standard deviation about that mean.

NaF) ions. Less precipitate is generated in like-hydrated (more associated) salts, in which nucleation rates of barite are higher, which suggests that Ω in these solutions is reduced more by nucleation and less by growth compared to precipitation in oppositely-hydrated salts and precipitate mass is added mainly by growth. The heat of barium sulfate precipitation (Q_{BaSO_4}) results from the net effect of nucleation and growth and generally increases with increasing amount of precipitate (Fig. 10).

However at lower Ω and lower IS conditions the dependence of Q_{BaSO_4} on the amount of precipitated solid follows different trends for like-hydrated and oppositely-hydrated background salts, with relative dominance of nucleation in the former and growth in the latter (Fig. 11).

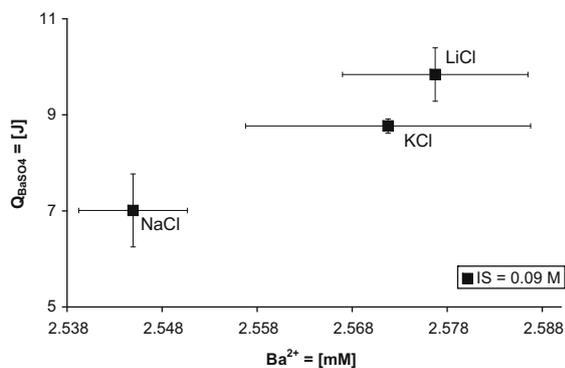


Fig. 10. Heat of barium sulfate precipitation (Q_{BaSO_4}) as a function of concentration of Ba^{2+} consumed during crystallization process at ionic strength (IS) = 0.09 M and supersaturation (Ω) = $10^{3.77}$. Q_{BaSO_4} and $[Ba^{2+}]$ represent average values from the precipitation experiments in the presence of the respective background salt, and the error bars represent one standard deviation about that mean.

Barite crystallization seems to be more exothermic in like-hydrated electrolytes (the trend line for Q_{BaSO_4} as a function of precipitate concentration is shifted towards higher values on the y-axis) which implies that nucleation gives a more positive heat signal than growth. Due to the significant experimental variability, the relationship based on the average values of Q_{BaSO_4} and $[Ba^{2+}]$ can be questioned. Nevertheless it was shown that the dependence of the rate of nucleation (this work) and growth (Kowacz and Putnis, 2008) of barite on properties of the electrolyte solution also follows different trends for like and oppositely-hydrated salts. This observation together with the fact that kinetics of nucleation and growth of barite change differently in response to the same changes in solution composition (Kowacz et al., 2007; Kowacz and Putnis, 2008) supports the suggestion that the energetical costs of these

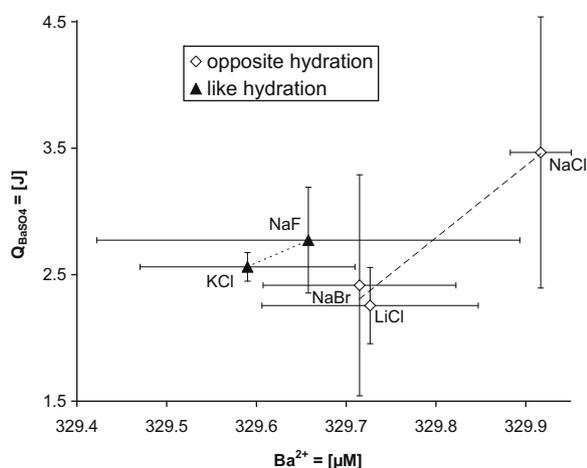


Fig. 11. Heat of barium sulfate precipitation (Q_{BaSO_4}) as a function of concentration of Ba^{2+} consumed during crystallization process at ionic strength (IS) = 0.03 M and supersaturation (Ω) = $10^{3.33}$. Q_{BaSO_4} and $[Ba^{2+}]$ represent average values from the precipitation experiments in the presence of the respective background salt, and the error bars represent one standard deviation about that mean.

elementary steps can be different. This can result from the proposed differences in the kinetic barriers for nucleation and ion addition at kinks (Kowacz and Putnis, 2008). Growth of barite was assumed to be limited by the energy required to remove water molecules hydrating the ion and the surface while nucleation is limited by the probability of contact of building units in a “dehydrated state” i.e. by the frequency of water exchange that determines dehydration rates and mobility of ions in solution. Therefore if we treat water exchange as a spontaneous thermal fluctuation (Zhang et al., 2007), the energetic costs of a nucleation event can be lower than that of ion attachment on the crystal surface. However, ion incorporation at kinks is more frequent because it is stabilized by strong electrostatic interactions with neighboring molecules within the crystal structure. Yet Coulombic forces can be insufficient to overcome the energy barrier of dehydration and stabilize the ion position on a flat terrace or next to another ion in solution.

4.4. Weakly hydrated ions and heterogeneous nucleation

The tendency of the structured solvent to exclude ions from its H-bonded network affects not only barite building units but also background ions present in solution. The solutions are undersaturated with respect to background salts, therefore those do not precipitate, but composing ions can associate in solution (Hawlicka and Swiatla-Wojcik, 2003) and separate from bulk water structure. Our findings suggest that such phenomena can have implications for heterogeneous nucleation of barite in solution.

In our experiments the size of barite crystals precipitated in different background sodium salts seems to be unaffected by changes in nucleation rates (as inferred from independence of size on β^2 at constant Ω) and for NaCl as a background electrolyte crystal size does not depend on supersaturation (for $\Omega = 10^{3.33}$ and $\Omega = 10^{3.47}$) (Fig. 5). Constant nucleus size regardless of increasing solution supersaturation (Ω) was observed for $BaSO_4$ precipitation in the presence of NaCl and interpreted as an indication of the dominant influence of heterogeneous nucleation (Kucher et al., 2006). At constant Ω , increasing nucleation kinetics should also result in precipitation of a higher amount of smaller particles. Therefore the independence of particle size on nucleation rates and on the saturation state of the solution observed in our experiments, implies the predominance of heterogeneous nucleation in the precipitation of the solid. This is consistent with the fact that the lower investigated supersaturation level ($\Omega = 10^{3.33}$) represents the borderline conditions between homogeneously and heterogeneously dominated nucleation of barite (He et al., 1995).

The experimental observation that Na^+ can be incorporated into the barite structure when present in solution as a salt of strongly hydrated anions (Kowacz and Putnis, 2008) suggests a possible explanation for the role of Na^+ in the nucleation process. Sodium incorporation was attributed to the fact that this weakly hydrated ion is preferentially excluded from the aqueous solvent with increasing solvent–solvent affinity. The tendency of an ion to separate from the bulk water structure leads to ion segregation at the

air/water interface (Jungwirth and Tobias, 2001, 2002; Garret, 2004; Ghosal et al., 2005; Manciu and Ruckenstein, 2005) or other interfaces (Collins, 1995) that can potentially serve as charged nucleation centers. The less hydrated the ion (the lower its charge to radius ratio) the higher the tendency to separate it from the structured aqueous solvent. Therefore the suggested mechanism for heterogeneous nucleation should be more strongly expressed with diminishing hydration of ions. This is in agreement with the experimental observation that barite nucleation rates in the heterogeneous region increase with increasing radius of monovalent ions ($\text{Na}^+ < \text{K}^+ < \text{Cs}^+ < (\text{CH}_3)_4\text{N}^+$) (He et al., 1995).

4.5. Solvent structure dynamics, kinetics of nucleation and crystal size

Control of the water structure dynamics on the kinetics of barite nucleation results in differences in the dependence of nucleation rates on supersaturation between solutions of background salts of distinct hydration characteristics (as inferred from changes of β^2 with Ω). This is expressed by only a minor increase in barite nucleation rates with increasing Ω in the chloride salt of negatively hydrated potassium, and a relatively sharp increase of nucleation kinetics in chloride salts of positively hydrated sodium and lithium (Fig. 5). Negatively hydrated K^+ ions reduce the affinity of water to other solvent molecules ($\tau_{0-\text{KCl}}$ decreases with concentration) which results in a higher degree of ordering of water molecules around a solute molecule immersed in KCl solution as the electrolyte concentration increases. On the contrary, positively hydrated Li^+ and Na^+ ions retard water mobility and therefore increase the average time that a solvent molecule spends in the bulk electrolyte solution ($\tau_{0-\text{NaCl}}$ and $\tau_{0-\text{LiCl}}$ increase with concentration) with respect to its residence time in the solute solvation shell. As a consequence, the frequency of water exchange around respective building units (i.e. the suggested rate-limiting factor for barium sulfate nucleation) increases with increasing KCl concentration and decreases with increasing LiCl and NaCl concentration in solution. This is in agreement with the respective changes in solution enthalpy of BaCl_2 (ΔH_{BaCl_2}) in solutions of different background electrolytes (Table 2). ΔH_{BaCl_2} expresses the relative differences between barium–water and water–water attractions, and therefore the enthalpy of solution data can indicate differences in the water exchange around Ba^{2+} in different background salts. At the same time the kinetic barrier for growth increases at higher IS in all background salts, due to electrostatic stabilization of water hydrating barite building units in solution and at crystal surface. This is expressed in the less negative enthalpy of precipitation at IS = 0.09 M (Table 1).

At higher Ω more material is brought into the reacting system, increasing the flux of ions into the surface and the probability of effective contact of building units in the bulk. Therefore growth and nucleation rates increase. Nevertheless because of the strong dependence of nucleation rate and critical nucleus size on supersaturation, the particle size is expected to diminish with increasing Ω . However in our experiments this is only the case with LiCl as a background

electrolyte, while in negatively hydrated KCl a significant increase in crystal size at higher supersaturation (and ionic strength) can be actually observed. For colloidal systems an increase in the crystallite size at larger supersaturations was recently attributed to the fact that the probability of formation of critical nuclei goes through a maximum as the Ω is increased because of the increase of solid–liquid interfacial tension (Auer and Frenkel, 2001), in contrast to the interpretation explaining crystal size as the effect of heterogeneous nucleation. Our findings suggest that the increase of barite particle size with increasing Ω can result from a solution-dependent kinetic barrier for nucleation which suppresses the dependence of nucleation rates on Ω . Furthermore, growth rates of barite (in the region where two-dimensional nucleation is not rate limiting) were suggested to be determined by the energetic costs of expelling waters of solvation and not by the frequency of water exchange (Kowacz and Putnis, 2008). It is worth noting that the residence time of water in an ion solvation shell can be relatively long, depending on the solvent structure dynamics, regardless of the weak electrostatic ion–water attractions (Koneshan et al., 1998). Because of the differences in kinetic barriers for nucleation and for ion attachment at kinks, growth can be more favored than nucleation at higher Ω , thus increasing crystal size. This can be the case in solutions where the dynamics of the aqueous solvent structure increases with Ω , for example as a result of addition of negatively hydrated solutes. Our observations are in agreement with other experimental results that have shown that increasing the concentration of the chloride salt of the negatively hydrated potassium ion increases the linear growth rate of barite, while chloride salts of positively hydrated sodium and calcium ions mainly increase nucleation rates (Matynia et al., 2004).

5. CONCLUSIONS

Our findings suggest that nucleation rates of barite and the resulting precipitate characteristics such as mean crystal size and crystal size variance can be modified by background salts present in solution, due to the effects of these electrolytes on the dynamics of the bulk aqueous solvent structure and on the water of solvation. The results presented here support the hypothesis that the frequency of water exchange, which determines the diffusion of ions in solution, is the kinetic barrier for the nucleation process of barium sulfate (Kowacz and Putnis, 2008). The resulting dependence of the nucleation kinetics on solvent structure dynamics allows the prediction of the effect of aqueous solvent properties on the crystallization process. Our results imply that weakening water–water interactions will suppress nucleation kinetics while increasing water affinity to other water molecules will assist nucleation kinetics. Our conclusions are consistent with experimental observations such as the enhanced nucleation rates of barite by addition of methanol (Tomson et al., 2005) which reduces water structure dynamics and consequently lowers the kinetic barrier of the cation desolvation (Piana et al., 2006). Identification of the kinetic barriers for crystal nucleation and growth and recognition of their dependence on solution composition suggests that it is possible to selectively control

fundamental steps in the crystallization process by adjusting solution composition. Such knowledge can add to our understanding of the influence of additives on crystal precipitation and should be helpful in designing a solvent with desirable impact on crystallization product characteristics.

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